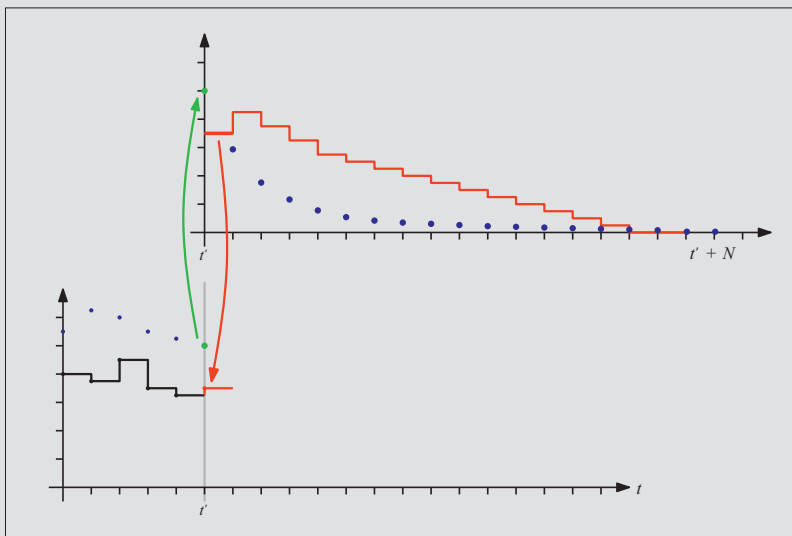


Bjarne Foss and  
Tor Aksel N. Heirung

# Merging Optimization and Control



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Department of Engineering Cybernetics  
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# Chapter 1

## Introduction

This text is intended as a basic introduction to optimization of dynamic systems, in particular Model Predictive Control (MPC). The material is a result of many years of teaching an undergraduate course in optimization and MPC at NTNU (Norwegian University of Science and Technology). Students taking this course have at least some familiarity with control systems, and in particular linear-systems theory at the level of Chen (1999). Key learning outcomes of this course are the ability to formulate appropriate engineering problems as mathematical optimization problems, and analyze and solve such optimization problems. Important optimization problem classes are presented and optimality conditions are discussed. Further, algorithms for solving optimization problems are treated, including some information on relevant software. This material is for the most part covered by the optimization textbook Nocedal and Wright (2006).

The second half of the course covers optimization of dynamic systems with a focus on MPC. Instead of using MPC textbooks written for a graduate-student audience, like Rawlings and Mayne (2009), Goodwin et al. (2004), Rossiter (2003), or Maciejowski (2002), we have written this note. The rationale is to provide a smooth transition from optimization to MPC via open loop optimal control. This approach is not taken in any available textbook on MPC. Rather than being a comprehensive treatment, the text is intended to explain the principles of MPC to undergraduates in an easy-to-grasp manner, better positioning the students to benefit from the more thorough treatments in the texts mentioned above.

The outline of this note is as follows. Section 2 repeats key concepts in optimization before Section 3 treats optimization of discrete time dynamic systems. This section shows how optimization based on static models easily can be extended to include dynamic time discrete models. This section introduces two important concepts, dynamic optimization and open loop

optimization. This provides a foundation for the optimal control section, in which the MPC concept is introduced. Section 4 discusses linear MPC, which is extensively used in practice. Linear quadratic control is an interesting case, which is treated separately. This section also includes material on state estimation, nonlinear MPC and comments related to practical use of MPC.

# Chapter 2

## Optimization

This section presents relevant background on optimization. It first classifies optimization problems and discusses some basic properties. Subsequently solution methods and computational issues are discussed. The notation mostly matches that of Nocedal and Wright (2006), which is also the basis for most of the material in this section.

### 2.1 Classes of optimization problems

*Mathematical optimization problems* include three main components, an *objective function*, *decision variables* and *constraints*. The objective function is a scalar function which describes a property that we want to minimize or maximize. The decision variables may be real variables, integers or binary variables, or belong to other spaces like function spaces. In this note the decision variables will mostly be limited to the *Euclidean space*, i.e., vectors of real variables. Constraints are normally divided into two types, *equality constraints* and *inequality constraints*. This background allows us to define an optimization problem, the *nonlinear program (NLP)*.

$$\min_{z \in \mathbb{R}^n} f(z) \tag{2.1a}$$

subject to

$$c_i(z) = 0, \quad i \in \mathcal{E} \tag{2.1b}$$

$$c_i(z) \geq 0, \quad i \in \mathcal{I} \tag{2.1c}$$

Some further explanation is required.  $f$  takes an  $n$ -dimensional vector and projects it onto the real axis. Further, the decision variables are defined on



a Euclidean space since  $z \in \mathbb{R}^n$  which excludes integer or binary decision variables.  $\mathcal{E}$  and  $\mathcal{I}$  are disjoint index sets, i.e.,  $\mathcal{E} \cap \mathcal{I} = \emptyset$ , for the constraints. Due to the constraints the decision variables  $z$  may be selected from a subset of  $\mathbb{R}^n$ . This subset is called the *feasible region* or the *feasible set* and is defined by the constraints  $c_i$ . More precisely the feasible set is defined by

$$\Omega = \left\{ z \in \mathbb{R}^n \mid (c_i(z) = 0, i \in \mathcal{E}) \wedge (c_i(z) \geq 0, i \in \mathcal{I}) \right\} \quad (2.2)$$

In some cases the feasible set may be further limited by the domain of  $f$  itself. A function like  $\sqrt{\cdot}$  is only defined for positive arguments. Such cases are, however, not considered in this note.

**Example 1** (Optimization problem and feasible area)

Consider the optimization problem

$$\min_{z \in \mathbb{R}^2} f(z) = z_1^2 + 3z_2 \quad (2.3a)$$

$$\text{s.t. } c_1(z) = z_1^2 + z_2^2 - 1 = 0 \quad (2.3b)$$

$$c_2(z) = z_1 + z_2 \geq 0 \quad (2.3c)$$

Here, we have that  $\mathcal{E} = \{1\}$  and  $\mathcal{I} = \{2\}$ . The feasible area for this problem is

$$\begin{aligned} \Omega &= \left\{ z \in \mathbb{R}^2 \mid c_1(z) = 0 \wedge c_2(z) \geq 0 \right\} \\ &= \left\{ z \in \mathbb{R}^2 \mid z_1^2 + z_2^2 = 1 \wedge z_1 + z_2 \geq 0 \right\} \end{aligned} \quad (2.4)$$

The feasible area  $\Omega$  is a half circle (not a half-disc) with radius 1, marked with red in Figure 2.1. △

The optimization problem in (2.1) is stated as a minimization problem. Some problems, where for instance the objective function represents profit, are clearly maximization problems. One should observe that any maximization problem can be translated into a minimization problem by observing that ‘ $\max f(z)$ ’ and ‘ $\min -f(z)$ ’ provide equal solutions apart from the opposite sign of the objective function value. The feasible set may be empty, i.e.,  $\Omega = \emptyset$ . In this case there is no solution, or no *feasible points*, to the optimization problem in (2.1).  $f(z)$  has to be bounded below for all feasible solutions meaning that  $f(z) \neq -\infty$  for all  $z \in \Omega$ . This has no practical consequence since all reasonable engineering problems will be constrained such that the objective function remains bounded.

A point  $z^* \in \Omega$  is the solution of (2.1) if

$$f(z^*) \leq f(z), \text{ for all } z \in \Omega$$

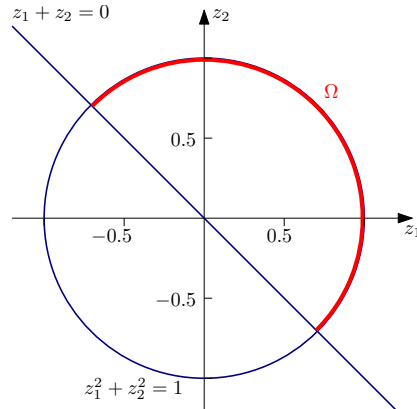


Figure 2.1: Feasible area (thick red curve) for Example 1.

Such a point is a *global minimizer*. There may be several such minimizing points. In the case of only one single global minimizer the global minimizer is a *strict global minimizer*. A *local minimizer*  $z^*$  provides a minimum value within some neighborhood rather than the whole feasible region and is defined by

$$f(z^*) \leq f(z), \text{ for all } z \in \|z - z^*\| < \epsilon$$

where  $z$  can take values in a feasible open set about  $z^*$ . A *strict local minimizer* is defined by replacing  $\leq$  with  $<$  above.

A key question is how to identify a minimization point. Provided certain smoothness conditions and regularity conditions are satisfied the *Karush-Kuhn-Tucker (KKT) conditions* define necessary conditions for optimality. First, however, we need to define the *Lagrange function* and *active constraints*.

$$\mathcal{L}(z, \lambda) = f(z) - \sum_{i \in \mathcal{E} \cup \mathcal{I}} \lambda_i c_i(z) \quad (2.5)$$

where  $\lambda_i$  are the *Lagrange multipliers*.

An active constraint is a constraint for which  $c_i(z) = 0$ , which implies that all equality constraints are active at a feasible point. An inequality constraint, however, may either be active or not active at a feasible point.

Since the KKT conditions is a key results in constrained optimization we state this result in some detail.

**Theorem 1** (First order necessary conditions).

*Assume that  $z^*$  is a local solution of (2.1) and that  $f$  and all  $c_i$  are differentiable and their derivatives are continuous. Further, assume that all the ac-*

tive constraint gradients are linearly independent at  $z^*$  (meaning that LICQ<sup>1</sup> holds). Then there exists Lagrange multipliers  $\lambda_i^*$  for  $i \in \mathcal{E} \cup \mathcal{I}$  such that the following conditions (called the KKT conditions) hold at  $(x^*, \lambda^*)$ ;

$$\nabla_z \mathcal{L}(z^*, \lambda^*) = 0 \quad (2.6a)$$

$$c_i(z^*) = 0, \quad i \in \mathcal{E} \quad (2.6b)$$

$$c_i(z^*) \geq 0, \quad i \in \mathcal{I} \quad (2.6c)$$

$$\lambda_i^* \geq 0, \quad i \in \mathcal{I} \quad (2.6d)$$

$$\lambda_i c_i(z^*) = 0, \quad i \in \mathcal{I} \quad (2.6e)$$

The KKT conditions are necessary conditions for a local solution. Sufficient conditions, however, can be derived through second order conditions.

**Theorem 2** (Second order sufficient conditions).

Suppose that for some feasible point  $z^* \in \mathbb{R}^n$  there exists Lagrange multipliers  $\lambda^*$  such that the KKT conditions (2.6) are satisfied, and that  $f$  and all  $c_i$  are twice differentiable and their derivatives are continuous. Assume also that

$$\nabla_{zz} \mathcal{L}(z^*, \lambda^*) \succ 0 \quad (2.7)$$

Then  $z^*$  is a strict local solution of (2.1).<sup>2</sup>

$\nabla_{zz} \mathcal{L}(z^*, \lambda^*)$  needs only be positive in certain directions, more specifically in directions defined by the *critical cone*<sup>3</sup>. Hence, the theorem above can be relaxed by requiring  $w^\top \nabla_{zz} \mathcal{L}(z^*, \lambda^*) w > 0$  where  $w \in \mathcal{C}(x^*, \lambda^*)$ . For further discussion on this we refer to Chapter 12 in Nocedal and Wright (2006).

A major divide in optimization is between *convex* and *nonconvex problems*. Convex problems hold the following key property.

*A local minimizer of a convex optimization problem is also a global minimizer.*

This implies that Theorem 1 provides necessary conditions and Theorem 2 sufficient conditions for a global solution for convex problems. It is therefore important to be able to identify convex problems.

An optimization problem is convex if it satisfies the following two conditions:

- *The objective function is a convex function.*

<sup>1</sup>LICQ stands for Linear Independence Constraint Qualification.

<sup>2</sup>The notation  $\succ 0$  means a positive definite matrix. Similarly,  $\succeq 0$ ,  $\prec 0$ , and  $\preceq 0$  mean positive semidefinite, negative definite, and negative semidefinite, respectively.

<sup>3</sup>The critical cone is loosely speaking directions that do not violate the constraints locally, see also Chapter 12 in Nocedal and Wright (2006).

- *The feasible set  $\Omega$  is a convex set.*

If a problem is *strictly convex* there will always only exist one (global) solution. For definitions of convex functions and convex sets we refer to Nocedal and Wright (2006).

We will now discuss some specific optimization problems defined by (2.1).

- If the objective function  $f$  is linear and all constraints  $c_i$  are linear, (2.1) is a *linear program (LP)* which is defined by

$$\min_{z \in \mathbb{R}^n} d^\top z \quad (2.8a)$$

subject to

$$c_i(z) = a_i^\top z - b_i = 0, \quad i \in \mathcal{E} \quad (2.8b)$$

$$c_i(z) = a_i^\top z - b_i \geq 0, \quad i \in \mathcal{I} \quad (2.8c)$$

Since all constraints are linear the feasible set is convex, and since  $f$  is linear it is also a convex function. Hence, LP problems are convex problems. LP problems are, however, not strictly convex since there may exist many solutions with equal optimal objective function values.

(2.8) can be formulated in various ways. In particular all LP problems can be written on the standard form which is shown below, see e.g., Chapter 13 in Nocedal and Wright (2006).

$$\min_{z \in \mathbb{R}^n} d'^\top z \quad (2.9a)$$

subject to

$$c'_i(z) = a'_i{}^\top z - b'_i = 0, \quad i \in \mathcal{E}' \quad (2.9b)$$

$$c'_i(z) = z_i \geq 0, \quad i \in \mathcal{I}' \quad (2.9c)$$

(2.8) and (2.9) are hence equivalent problems provided all vectors and sets are chosen appropriately. It may be noted that a constant term may be added to (2.8) or (2.9) without changing the solution except for the optimal objective function value. Hence, such a bias term is usually removed.

It is worth mentioning that the KKT conditions are both necessary and sufficient conditions for the LP problem. Moreover, since the LP problem is convex the KKT conditions define a global solution.

- When the objective function  $f$  is a quadratic function and all constraints  $c_i$  are linear, (2.1) is a *quadratic program (QP)* which is defined by

$$\min_{z \in \mathbb{R}^n} z^\top Qz + d^\top z \quad (2.10a)$$

subject to

$$c_i(z) = a_i^\top z - b_i = 0, \quad i \in \mathcal{E} \quad (2.10b)$$

$$c_i(z) = a_i^\top z - b_i \geq 0, \quad i \in \mathcal{I} \quad (2.10c)$$

Again all constraints are linear. Hence, the feasible set is convex. A constant term may be added to (2.10a). QP problems may be convex or nonconvex depending on the quadratic form  $z^\top Qz$  and the constraints.  $Q$  is an  $n$ -dimensional symmetric matrix and the following statement holds.

- *If  $Q$  is positive semidefinite, i.e.,  $Q \succeq 0$ , then (2.10) is a convex problem.*

It may be noted that  $Q = 0$  is a positive semidefinite matrix. In this case (2.10) turns into a LP problem which indeed is a convex problem. The  $Q \succeq 0$  condition may be relaxed as follows, see also Chapter 16 in Nocedal and Wright (2006).

- *If  $Z^\top QZ$  is positive semidefinite where  $Z$  spans the null space of the active constraints, then (2.10) is a convex problem.*

The KKT conditions are both necessary and sufficient conditions for a convex QP problem. Moreover, the KKT conditions define a global solution in this case.

- If the objective function  $f$  is a convex function, all the equality constraints are linear and  $-c_i$  are convex functions for  $i \in \mathcal{I}$ , then (2.1) is a *convex programming* problem. Hence, the optimization problem is convex. It is useful to note that nonlinear equality constraints always give rise to nonconvex problems.
- If there are no constraints, i.e., both  $\mathcal{E}$  and  $\mathcal{I}$  are empty sets, (2.1) is an *unconstrained problem* meaning that  $\Omega = \mathbb{R}^n$ .
- If the objective function is some arbitrary nonlinear function or the constraints  $c_i$  are nonlinear functions, then (2.1) is a nonconvex problem.

Sketches of convex and nonconvex sets are shown in Figure 2.2 while convex and nonconvex functions are depicted in Figure 2.3. Note that the region above the graph of a convex function is a convex region, and that the region above the graph of a nonconvex function is a nonconvex region.



Figure 2.2: Comparison of a convex and a nonconvex set.

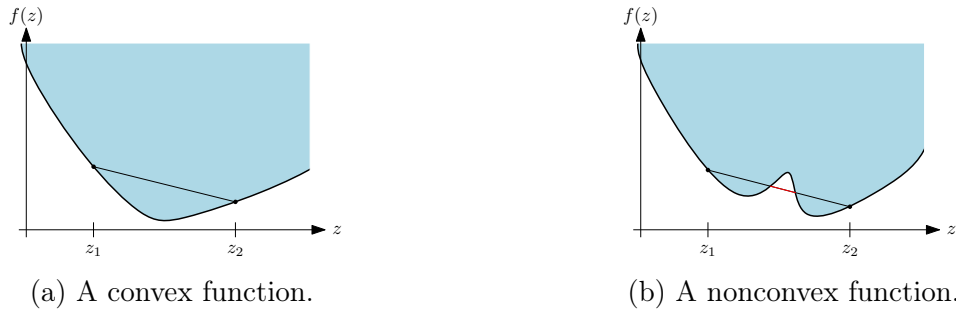


Figure 2.3: Comparison of a convex and a nonconvex function.

For completeness some comments on mixed integer formulations are included. A *mixed integer nonlinear program* (MINLP) is defined by

$$\min_{z \in \mathbb{R}^n, y \in \mathbb{Z}^q} f(z, y) \quad (2.11a)$$

subject to

$$c_i(z, y) = 0, \quad i \in \mathcal{E} \quad (2.11b)$$

$$c_i(z, y) \geq 0, \quad i \in \mathcal{I} \quad (2.11c)$$

where  $\mathbb{Z}^q$  defines a vector of integer variables. It is quite common to replace integer variables by binary variables, i.e.,  $y \in \{0, 1\}^q$ . By the definition of convex sets (2.11) is always a nonconvex problem since  $\mathbb{Z}^q$  is a disconnected set. Integer variables are useful to describe discrete decisions such as a routing decision. One example is a stream which can be routed to one out of two

pipelines and a second example are on-off valves, which are either fully open or closed. An important sub-class of problems are *mixed integer linear programs* (*MILP*) where the problem is convex except for the integer variables. Another important class of problems are *integer programs* (*IP*) with only discrete decision variables meaning that  $z$  is removed from (2.11) (Nemhauser and Wolsey, 1999).

## 2.2 Solution methods

Solution methods for optimization problems do in principle vary from explicit solution to complex iterative schemes. Explicit solutions are however only available for some simple problems. We will encounter one such relevant problem later, namely the *linear quadratic control* (*LQ*) problem. Otherwise the solution approach is always an iterative algorithm. There are different ways of categorizing such algorithms. We will start of by describing the structure of many such algorithms.

---

### Algorithm 1 Iterative solution procedure

---

Given initial point  $z_0$  and termination criteria  
**while** termination criteria not satisfied **do**  
    Compute the next iteration point  
**end while**

---

Iterative algorithms need an initial value for  $z$  to start off. Some algorithms require a feasible initial point while this is no requirement for other algorithms. The well known *Simplex method* for solving LP problems and the active set method for solving QP problems require an initial feasible point while for instance the sequential quadratic programming (SQP) method does not require an initial feasible point.

Algorithms also need termination criteria<sup>4</sup>. These will include one or several of the following criteria: (i) a maximum allowed number of iterations, (ii) one or several progress metrics, and (iii) a characterization of the optimal point. A progress metric may be the change in objective function value, its gradient ( $\nabla f$ ), or the gradient of the Lagrange function ( $\nabla \mathcal{L}$ ) from one iteration to the next. Optimal points may be characterized by  $\|\nabla f\| < \epsilon$  or  $\|\nabla \mathcal{L}\| < \epsilon$  where  $\epsilon > 0$  is a small number.

Item 2 in Algorithm 1 is usually the most extensive point and there are a variety of methods. A large class of methods are gradient based methods in

---

<sup>4</sup>Also called stopping criteria.

which the new iteration point uses gradient information to compute a new iterate according to the following scheme.

$$z_{k+1} = z_k + \alpha_k p_k \quad (2.12)$$

$k$  denotes the iteration number, while  $p_k \in \mathbb{R}^n$  is the search direction and  $\alpha_k \in \mathbb{R}_+$  is a positive *line search* parameter. The search direction  $p_k$  depends on gradient information. Several alternatives exist, one alternative being the *steepest descent direction* in which  $p_k = -\nabla f(z_k)$  and the *Newton direction* where  $p_k = -(\nabla_{zz}f(z_k))^{-1}\nabla f(z_k)$ . In the latter case  $\nabla_{zz}f$  is the *Hessian* of  $f$ . A key point in all gradient based schemes is that  $p_k$  points in a descent direction for  $f(z_k)$ . Therefore the *directional derivative* should be negative, i.e.,  $\nabla f(z_k)p_k < 0$ . It should be noted that both the derivative and Hessian information is required in Newton schemes. In practice, however, a Quasi-Newton method is usually applied which means that the Hessian matrix is approximated, i.e.,  $B_k \approx \nabla_{zz}f(z_k)$ , and  $p_k = -B_k^{-1}\nabla f(z_k)$ . The calculation of  $B_k$  will be fast compared to the Hessian matrix since  $B_k$  uses gradient information only. Further, positive definiteness of  $B_k$  can be controlled. The latter is important since  $B_k \succ 0$  implies that  $-B_k^{-1}\nabla f(z_k)$  is a descent direction. A robust and efficient Quasi-Newton algorithm, which computes  $B_k^{-1}$ , is the *BFGS algorithm*.

Gradients can be computed using finite differencing and automatic differentiation. Finite differencing is based on Taylor's theorem and the gradient is estimated using perturbations. Approximation accuracy varies. A central difference scheme is for instance more accurate than forward differencing. The computation time for the former is, on the other hand, roughly the double of the latter. Accuracy also depends on the perturbation size. Automatic differentiation is an efficient way of computing derivatives. It basically adopts the chain rule by dividing complex functions into elementary operations. This approach is gaining popularity and is gradually implemented in optimization packages, see also Chapter 8 in Nocedal and Wright (2006) for more information.

Some methods exploit structural properties in order to compute the next iteration point. This is the case for the Simplex method, which uses the fact that it is sufficient to look for a solution in vertexes of the feasible polytope given by the linear constraints in LP problems. Hence, the iterates  $z_k$  jump from one feasible vertex to another until the KKT conditions, which are both necessary and sufficient conditions for a solutions, are met.

There are many *derivative free methods* (Conn et al., 2009), i.e., methods where no explicit gradient information is used in the search. These methods can be divided into two main groups, *pattern search methods* and *model based*



*methods.* Examples of pattern search techniques are the Hooke Jeeves direct search (Hooke and Jeeves, 1961), the Nelder-Mead algorithm (Conn et al., 2009), generalized pattern search (Torzcon, 1997) and the mesh adaptive direct search (Audet and Dennis JR., 2006). These methods are applicable to problems with a limited number of decision variables, typically less than a few hundred optimization variables. They are, however, fairly easy to implement in a distributed computing environment, a measure that improves efficiency. Model based methods approximate  $f$  in the vicinity of  $z_k$  by a simple, typically quadratic, model. These methods are called trust region derivative free methods, cf. Conn et al. (2009). An advantage of the trust region methods is that it is possible to establish stringent convergence proofs for these algorithms.

Derivative-free methods are popular since they are easily understood and straightforward to implement. To elaborate further, evaluating the objective function will in some cases require extensive computations. This is for instance the case if the equality constraints are embedded in a simulator. One example, among many, is a simulator of the electricity grid in Southern Norway where the decision variables are capacitors placed in different locations of the grid. The objective would typically be to keep the voltage within upper and lower bounds by changing the capacitor load. In this case the simulator must be run once in order to compute the objective function once. Now, simulators do not usually supply gradients. Hence, one may be forced to use a derivative free method. To reiterate, a parallel implementation in this case may reduce runtime significantly.

# Chapter 3

## Optimization of dynamic systems

*Dynamic systems* are characterized by changes over time which means that variables are functions of time. On the other hand, *static systems* are time independent. Dynamic systems are modeled in many different ways, for instance with differential equations, and there are different approaches to optimization of such systems. Two main categories, *quasi dynamic optimization* and *dynamic optimization*, are explained below.

- Quasi dynamic optimization: Optimize a dynamic system by repetitive optimization on a static model. The idea is that the dynamic changes can be compensated for by frequent reoptimizing on a static model. This approach works well for slowly varying systems and systems that are mostly in steady state.
- Dynamic optimization: Optimize on a dynamic model. In this case the solution will be a function of time, i.e., all decision variables will be functions of time. Dynamic optimization is necessary when dynamics plays a major role, which quite often is the case for systems with frequent changes in the operating conditions.

This note will focus on dynamic optimization. Before discussing this, however, we illustrate an example of quasi dynamic optimization.

### **Example 2** (Optimizing oil production)

Assume that 5 wells are producing according to the sketch in Figure 2. The well streams contain gas, oil and water. Further, the mass fraction of gas, oil and water in a well varies slowly with time. Hence, a well will produce according to

$$q_i(t) = a_{gi}(t)q_{gi}(t) + a_{oi}(t)q_{oi}(t) + a_{wi}(t)q_{wi}(t), \quad i = 1, \dots, 5$$

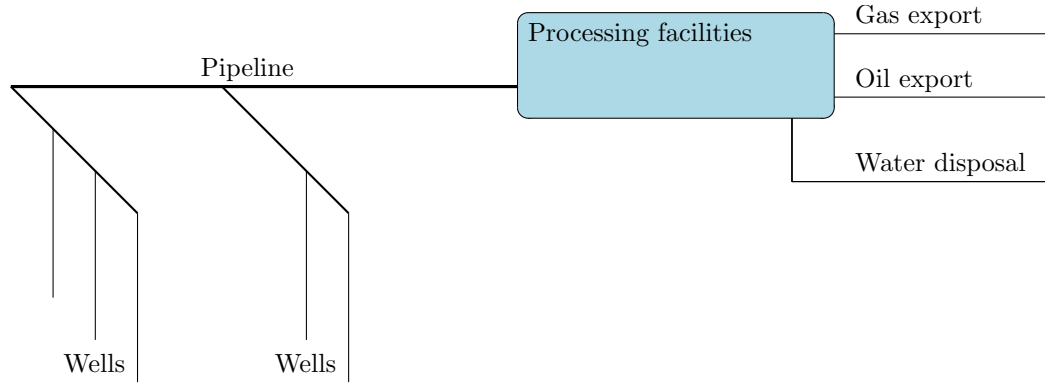


Figure 3.1: Sketch of oil production system for Example 2.

where  $t$  defines time.  $q_i(t)$  is the total rate from well  $i$  while  $q_{gi}(t)$ ,  $q_{oi}(t)$ ,  $q_{wi}(t)$  are gas, oil and water rates, respectively. Since we use mass rates the mass fractions always add up to one, i.e.,  $a_{gi}(t) + a_{oi}(t) + a_{wi}(t) = 1$ .

Assume that the goal is to maximize oil production while honoring operational constraints like gas processing and water processing capacities on a platform, and rate limits in each well. This may be formulated as an LP problem as in (2.8).

$$\min_{z \in \mathbb{R}^{20}} (0, 0, -1, 0, \dots, 0, 0, -1, 0)z \quad (3.1a)$$

subject to

$$q_i(t) - a_{gi}(t)q_{gi}(t) - a_{oi}(t)q_{oi}(t) - a_{wi}(t)q_{wi}(t) = 0, \quad i = 1, \dots, 5 \quad (3.1b)$$

$$a_{gi}(t) + a_{oi}(t) + a_{wi}(t) = 1, \quad i = 1, \dots, 5 \quad (3.1c)$$

$$q_i(t) \leq q_i^{\max}, \quad i = 1, \dots, 5 \quad (3.1d)$$

$$q_{g1}(t) + \dots + q_{g5}(t) \leq q_{\text{gas}}^{\max} \quad (3.1e)$$

$$q_{w1}(t) + \dots + q_{w5}(t) \leq q_{\text{water}}^{\max} \quad (3.1f)$$

$$z \geq 0 \quad (3.1g)$$

where

$$z = (q_1, q_{g1}, q_{o1}, q_{w1}, \dots, q_5, q_{g5}, q_{o5}, q_{w5})^\top \quad (3.1h)$$

This is a simple LP problem, which is easily solved. One interesting question, however, is how to account for variations in time. One approach is to take a snapshot at a given time  $t_0$  and solve (3.1) assuming static conditions, i.e, constant mass fractions. This solution is denoted by  $z^*(t_0)$ . After some time, i.e.,  $t_1 > t_0$ , the mass fractions may have changed significantly, thus,

$z^*(t_0)$  is no longer an (optimal) solution and it may even be infeasible. Hence, a new solution  $z^*(t_1)$  is computed. A valid strategy is therefore to compute a new solution once the mass fractions have changed significantly<sup>1</sup>.

A second approach is to treat the problem as a dynamical system. Let us assume that the flow dynamics associated with changes in flow rates are important. One operational example of the latter is during start up of a well, i.e., starting production after the well has been closed in for some time. Such a start up may take several hours. This behavior is not included in the description above since it requires a model with flow dynamics. Such a model may for instance be based on differential equations.  $\triangle$

We will from now on only consider dynamic optimization and start by categorizing these problems by model type and control parametrization, i.e., how the control input is defined. Model formats are many and range from differential or differential algebraic (DAE) systems to transfer functions and further *state space models*. In this note we use state space models, see e.g., Chen (1999), since this is a fairly general class of system and such models are frequently used in dynamic optimization. The presentation is limited to discrete time models since continuous time models require quite different solution methods.

### 3.1 Discrete time models

A discrete time system is sampled at discrete points in time. These sampling points are usually equidistant in time. Such a system can be described by a finite difference model in the following form

$$x_{t+1} = g(x_t, u_t) \tag{3.2a}$$

where system dimensions are given by

$$u_t \in \mathbb{R}^{n_u} \tag{3.2b}$$

$$x_t \in \mathbb{R}^{n_x} \tag{3.2c}$$

The function  $g$  maps an  $(n_u + n_x)$ -dimensional vector onto  $\mathbb{R}^{n_x}$ . The subscript  $t$  is a discrete time index. A slightly more general model is obtained if  $g$  is an explicit model in time, i.e.,  $g_t(x_t, u_t)$ . The control input  $u_t$  is assumed to be piecewise constant, i.e., it is constant on the continuous time  $[t, t + 1)$ , and hence the change from  $u_t$  to  $u_{t+1}$  occurs in a stepwise manner at  $t + 1$ .

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<sup>1</sup>The meaning of “significantly” in terms of a quantitative measure will have to be chosen in each individual case.

As opposed to the control inputs the states  $x_t$  are only defined at discrete points in time, and not in between these sampling points.

*Note that subscript  $t$  is used above.* It refers to discrete time, i.e., discrete points in time, as opposed to subscript  $k$  which is used as an iteration index, see e.g., (2.12).

The linear equivalent of (3.2) is obtained by replacing  $g$  with a linear function,

$$x_{t+1} = Ax_t + Bu_t \quad (3.3)$$

Equation (3.3) represents a *linear time invariant (LTI)* system since the matrices  $A$  and  $B$  are constant while the more general formulation below shows a *linear time variant (LTV)* since  $A$  and  $B$  are functions of time.

$$x_{t+1} = A_t x_t + B_t u_t \quad (3.4)$$

The LTV and LTI models are often used since nonlinear systems may be approximated by linear ones. The link between (3.2) and the linear models is established by the following approximation.

Assume that  $\bar{x}_t, \bar{u}_t$  is a stationary point for  $g$

$$x_{t+1} = \bar{x}_t = g(\bar{x}_t, \bar{u}_t) \quad (3.5)$$

and that  $g$  is at least one time differentiable. Further, define a perturbation about the stationary point by  $\delta x_t, \delta u_t$ . This situation may be approximated, or modeled, using a first-order Taylor series expansion.

$$\begin{aligned} x_{t+1} &= g(x_t, u_t) = g(\bar{x}_t + \delta x_t, \bar{u}_t + \delta u_t) \\ &\approx g(\bar{x}_t, \bar{u}_t) + \frac{\partial g(\bar{x}_t, \bar{u}_t)}{\partial x_t} \delta x_t + \frac{\partial g(\bar{x}_t, \bar{u}_t)}{\partial u_t} \delta u_t \end{aligned}$$

By defining a perturbation on the next state  $x_{t+1} = \bar{x}_t + \delta x_{t+1}$  we obtain the following expression

$$x_{t+1} = \bar{x}_t + \delta x_{t+1} \approx g(\bar{x}_t, \bar{u}_t) + \frac{\partial g(\bar{x}_t, \bar{u}_t)}{\partial x_t} \delta x_t + \frac{\partial g(\bar{x}_t, \bar{u}_t)}{\partial u_t} \delta u_t$$

which reduces to

$$\delta x_{t+1} \approx \frac{\partial g(\bar{x}_t, \bar{u}_t)}{\partial x_t} \delta x_t + \frac{\partial g(\bar{x}_t, \bar{u}_t)}{\partial u_t} \delta u_t \quad (3.6)$$

This is equivalent to an LTV model if we replace the *Jacobian matrices*, i.e.,  $\frac{\partial g(\bar{x}_t, \bar{u}_t)}{\partial x_t}$  and  $\frac{\partial g(\bar{x}_t, \bar{u}_t)}{\partial u_t}$ , by  $A_t$  and  $B_t$ , and define  $\delta x_t$  as the states and  $\delta u_t$  as the control inputs. A few observations are however in order:

- If  $g$  is highly nonlinear the linear approximation (3.6) will be poor. Hence, it makes sense to use the nonlinear model (3.2) in such cases.
- If  $g$  is mildly nonlinear (3.6) may suffice.
- If  $g$  is mildly nonlinear and the the range in which  $x_t$  and  $u_t$  varies is small, an even coarser approximation than (3.6) may be used, namely an LTI model like in (3.3).

The discussion above may be repeated for non-stationary points by replacing (3.5) with  $\bar{x}_{t+1} = g(\bar{x}_t, \bar{u}_t)$  and  $x_{t+1} = \bar{x}_{t+1} + \delta x_{t+1}$ .

## 3.2 Objective functions for discrete time systems

The dynamic optimization problem always stretches over time meaning that the objective function will include time. We therefore define the following objective function.

$$f(x_1, \dots, x_N, u_0, \dots, u_N) = \sum_{t=0}^{N-1} f_t(x_{t+1}, u_t) \quad (3.7)$$

This objective function will now be explained.

- The objective function is defined on a time horizon from  $t = 0$  to  $t = N$  where subscript  $t$  is the discrete time index. The time span from 0 to  $N$  is called the *prediction horizon*. It should be noted that it is straightforward to replace the prediction horizon by a time horizon which starts at time  $t = j$  and continues until  $t = j + N$ . In this note we assume equidistant times, i.e., all the sampling times are equal.
- The number of decision variables  $(x_1, \dots, x_N, u_0, \dots, u_N)$  increases linearly with the prediction horizon  $N$ .
- The objective function is structured such that it sums the contributions from each time step through  $f_t(x_{t+1}, u_t)$ .
- The initial state  $x_0$  is not a decision variable since it is assumed to be given. It is either known exactly or it may be estimated.  $x_{t+1}$  is the state at the end of the control interval for  $u_t$ , i.e., at the end of the continuous time interval  $[t, t + 1)$ . This is why we pair  $x_{t+1}, u_t$  and therefore use  $f_t(x_{t+1}, u_t)$  instead of  $f_t(x_t, u_t)$ .

- $f_t$  may focus on different types of desired properties. Some examples are mentioned below.
  - Economic measures like revenue and cost may be maximized or minimized over the time horizon. One example is an objective function which minimizes the energy consumption of an airplane or a ship on its journey between two destinations. Another example could be minimizing energy use in a building.
  - A system may need to follow a reference trajectory. Examples include a vessel that needs to follow a prescribed route, or a batch chemical reactor where the temperature profile over time is critical for product quality.
  - A system should reach a given state at the end of the time horizon. An example is a rocket that should reach a certain altitude.
  - Limit wear and tear on equipment while honoring operational constraints. An example is minimizing valve movements while maintaining required control performance.

There are problems which are not covered by (3.7), e.g., the minimal time case. An example of the latter is a fighter plane that should move from one location to another as fast as possible. In this case the prediction horizon  $N$  also becomes a decision variable.

### 3.3 Dynamic optimization with linear models

Given the options above a variety of dynamic optimization problems may be formulated. We start off with linear models and assume a quadratic objective function since this is a commonly used formulation.

Objective function (3.7) may now be written as

$$f(z) = \sum_{t=0}^N f_t(x_{t+1}, u_t) = \sum_{t=0}^{N-1} \frac{1}{2} x_{t+1}^\top Q_{t+1} x_{t+1} + d_{x_{t+1}}^\top x_{t+1} + \frac{1}{2} u_t^\top R_t u_t + d_{u_t}^\top u_t$$

with  $Q_t \succeq 0$  and  $R_t \succeq 0$ , which gives rise to the following QP problem.<sup>2</sup>

$$\min_{z \in \mathbb{R}^n} f(z) = \sum_{t=0}^{N-1} \frac{1}{2} x_{t+1}^\top Q_{t+1} x_{t+1} + d_{x_{t+1}}^\top x_{t+1} + \frac{1}{2} u_t^\top R_t u_t + d_{u_t}^\top u_t \quad (3.8a)$$

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<sup>2</sup>It is common to include  $\frac{1}{2}$  as a part of the quadratic terms in dynamic optimization. The reason is that some results, in particular linear quadratic control (LQ), which will be discussed later, uses this convention.

subject to

$$x_{t+1} = A_t x_t + B_t u_t, \quad t = 0, \dots, N-1 \quad (3.8b)$$

$$x_0, u_{-1} = \text{given} \quad (3.8c)$$

$$x^{\text{low}} \leq x_t \leq x^{\text{high}}, \quad t = 1, \dots, N \quad (3.8d)$$

$$u^{\text{low}} \leq u_t \leq u^{\text{high}}, \quad t = 0, \dots, N-1 \quad (3.8e)$$

$$-\Delta u^{\text{high}} \leq \Delta u_t \leq \Delta u^{\text{high}}, \quad t = 0, \dots, N-1 \quad (3.8f)$$

where

$$Q_t \succeq 0 \quad t = 1, \dots, N \quad (3.8g)$$

$$R_t \succeq 0 \quad t = 0, \dots, N-1 \quad (3.8h)$$

$$\Delta u_t = u_t - u_{t-1} \quad (3.8i)$$

$$z^\top = (x_1^\top, \dots, x_N^\top, u_0^\top, \dots, u_{N-1}^\top) \quad (3.8j)$$

$$n = N \cdot (n_x + n_u) \quad (3.8k)$$

In the interest of simplifying the notation, we will not specify the set of times  $t$  for the constraints whenever a special case of (3.8) is stated later in this note.

Several comments are included to explain the formulation.

- The reason for using index  $t+1$  for the states  $x_t$  is that the states of interest are  $x_1, \dots, x_N$  since  $x_0$  is fixed. This is different for the control input since  $u_0$  defines the control on the time interval  $[0, 1)$  and  $u_{N-1}$  the control on  $[N-1, N)$ . Hence, we cover the whole prediction horizon.
- The discrete time model appears as an equality condition in the optimization problem. Further, we observe that it is repeated  $N$  times, once for each time step on the horizon. The reason why  $t$  runs only to  $N-1$  is the fact that  $x_N$  is given by information at time  $N-1$  since  $x_N = A_{N-1}x_{N-1} + B_{N-1}u_{N-1}$ .
- An initial value  $x_0$ , i.e., the state at the beginning of the prediction horizon, is required. It is given as an equality constraint meaning that  $x_0$  is no free variable for optimization.
- Similarly,  $u_{-1}$  is a parameter in the optimization problem. We need the previous input  $u_{-1}$  in order to calculate  $\Delta u_0 = u_0 - u_{-1}$  which is constrained in (3.8f). In cases where we have no constraints on  $\Delta u_t$ , we do not need the  $u_{-1}$  in the optimization problem. Note that  $u_{-1}$  is the control applied to the plant at the previous time step; that is,



the time step right before the beginning of our current horizon. We can think of this as feedback from both the state  $x$  and the previous control input  $u_{-1}$ . This can be achieved by augmenting the state vector with the extra state  $x_{n_x+1} = u_{-1}$  when  $\Delta u_t$  is included in the formulation.

- Upper and lower bounds are placed on the states. These could be temperature or pressure limits, or for instance speed constraints. The constraints are repeated  $N$  times while no limit is set on  $x_0$  since it is given by (3.8c).  $x^{\text{low}}$  and  $x^{\text{high}}$  are vectors and if no specific limits exists for certain states the corresponding elements of  $x^{\text{low}}$  and  $x^{\text{high}}$  may be set to  $-\infty$  and  $+\infty$ , respectively.
- Constraint (3.8d) may well be generalized by placing limits on some controlled variable  $\gamma_t$  instead of the states, i.e., by replacing  $x_t$  with  $\gamma_t = h(x_t)$  and constraining this function. An example of the latter may be limits on product quality, say viscosity of paint, which can be modeled as a function of the states which may include temperature, humidity and concentration of certain species. If  $h$  is a linear function then  $\gamma_t = Hx_t$ .
- The objective function (3.8a) may weight the controlled variable  $\gamma_t$  instead of  $x_t$ . For a linear model,  $\gamma_t = Hx_t$ , the objective function is then given by

$$\begin{aligned} f(z) &= \sum_{t=0}^{N-1} \frac{1}{2} \gamma_{t+1}^\top Q_{t+1} \gamma_{t+1} + d_{\gamma_{t+1}}^\top \gamma_{t+1} + \frac{1}{2} u_t^\top R_t u_t + d_{u_t}^\top u_t \\ &= \sum_{t=0}^{N-1} \frac{1}{2} x_{t+1}^\top H^\top Q_{t+1} H x_{t+1} + d_{\gamma_{t+1}}^\top H x_{t+1} + \frac{1}{2} u_t^\top R_t u_t + d_{u_t}^\top u_t \quad (3.9) \end{aligned}$$

where  $H^\top Q_{t+1} H$  replaces  $Q_{t+1}$  in (3.8a). In this case we typically choose  $Q_t \succ 0$  since  $\gamma_t$  has been selected to include only important controlled variables.

- The objective function is of LTV type since  $Q_t$  and  $R_t$  are time varying. It is common to use an LTI objective where these matrices do not vary with time.
- The control input is limited by upper and lower bounds. An obvious example of this is a valve with a range from closed to fully open. The control input constraints run from 0 till  $N - 1$  since  $u_{N-1}$  defines the control input on the time horizon  $t \in [N - 1, N)$ .

- The change in the control input is restricted by (3.8f). This is very often an issue since for instance valves or motors do have limits on their dynamic performance, i.e., the speed with which the control input may change.
- (3.8) is called an *open loop optimization problem* since it does not include feedback control. Feedback control is a central topic in Section 4.

Discrete time models usually have many more states than control inputs, i.e.,  $n_x \gg n_u$ . Hence, the number of decision variables are essentially governed by the state dimension and the prediction horizon  $N$ . An example of a typical size could be  $N = 20$ ,  $n_x = 25$ ,  $n_u = 4$  meaning that the number of decision variables is 580 since  $n = N \cdot (n_x + n_u) = 20 \cdot (25 + 4) = 580$ . According to (3.8b) and (3.8c), there are 525 equality constraints. Viewing this from a control viewpoint the future state trajectory  $x_1, \dots, x_N$  is given by the initial state  $x_0$  and the control trajectory  $u_0, \dots, u_{N-1}$  through the discrete time model. Therefore the states may be eliminated by substituting  $x_0, \dots, x_N$  in the objective function and the state constraints with  $u_0, \dots, u_{N-1}$  using (3.8b) and (3.8c). At the end we are then left with  $20 \times 4 = 80$  decision variables instead of 580. There is a penalty to be paid, however, since in the latter reduced-space case, the resulting constraint matrices (see Ch. 16 in Nocedal and Wright (2006)) are dense, while in the full-space formulation they are sparse<sup>3</sup>. All modern optimization codes include linear algebra routines to utilize sparsity in the constraint matrices.

We have so far studied how a dynamic optimization problem can be converted into a QP problem. Two important questions still need attention. First, why is the quadratic objective function a reasonable option and, second, will (3.8) be a convex QP problem?

The quadratic objective function (3.8a) is a reasonable option and it is by far the most widely used objective function. Reasons for these are:

1. Economic measures like revenue or cost are often linear in one or several states and one or several control inputs, respectively. The typical structure of such terms are thus  $d_{xt}x_t$  and  $d_{ut}u_t$  where  $d_{xt}$  and  $d_{ut}$  include sales prices and the cost of input factors, respectively. This is a special case of (3.8a).
2. A system may need to follow a reference trajectory, one example being a vessel which has been issued a prescribed route. In this case the

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<sup>3</sup>In a sparse matrix the majority of elements are 0.

following term where  $Q \succeq 0$  makes sense

$$\frac{1}{2}(x_t - x_t^{\text{ref}})^\top Q(x_t - x_t^{\text{ref}}), \quad Q \succeq 0 \quad (3.10a)$$

This term can be rewritten as

$$\frac{1}{2}x_t^\top Qx_t - (x_t^{\text{ref}})^\top Qx_t + \frac{1}{2}(x_t^{\text{ref}})^\top Qx_t^{\text{ref}} \quad (3.10b)$$

Hence, in the tracking case the objective function term includes a quadratic term, a linear term, and a constant. Often we replace  $x_t$  by the output variable  $\gamma_t$ , which was discussed in conjunction with (3.9), and which does not change the problem structure.

There is one common extension to (3.8a), which is to include the following term

$$\frac{1}{2}\Delta u_t^\top R_{\Delta t}\Delta u_t \quad (3.11)$$

with  $R_{\Delta t} \succ 0$ . This penalizes *control moves*<sup>4</sup> and thereby wear and tear on actuators like valves.

In dynamic optimization  $Q_t$  in (3.8) will almost always be diagonal. Further, it is always positive semidefinite. The same holds for  $R_t$  and  $R_{\Delta t}$ .

*The conclusion from the above discussion is that a convex QP problem, or alternatively an LP problem, is a useful formulation in dynamic optimization.* Hence, the theory and solution methods discussed in Chapter 16 in Nocedal and Wright (2006), and in Chapter 13 for LP problems, do indeed provide an excellent platform for solving dynamic optimization problems.

An interesting observation is that the use of an LTI or LTV model in (3.8) is quite similar from a solution point of view. In both cases the problem is convex. The only difference is that the linear model calculations in (3.6) are more involved in the LTV case since  $A_0, \dots, A_{N-1}, B_0, \dots, B_{N-1}$  are required instead of just  $A, B$ . This may be an important difference if each Jacobian matrix computation is demanding.

### 3.4 The choice of objective function in optimal control

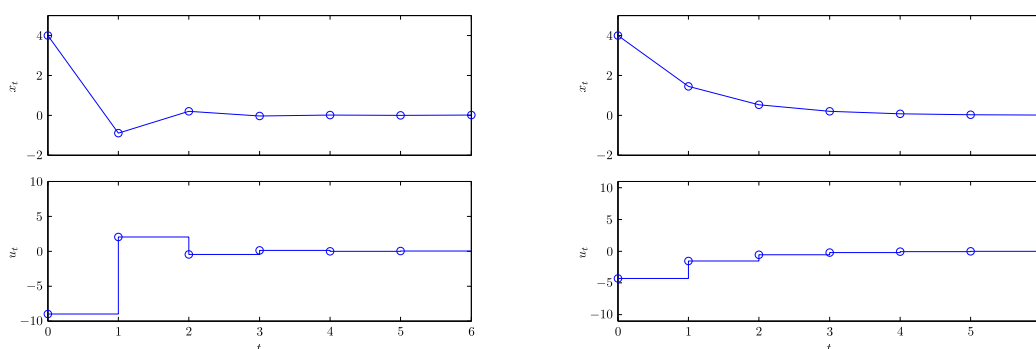
In the following two subsections we will discuss the choice of objective function and its links to closed loop system performance. Further, we provide

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<sup>4</sup>A control move is defined by  $\Delta u_t = u_t - u_{t-1}$ .

some examples. The discussion will be quite concrete and for simplicity center on *SISO* systems<sup>5</sup>.

Consider the two sets of system and control trajectories in Figure 3.2. For both of these cases, the state reference point for the controllers is  $x_t^{\text{ref}} \equiv 0$ . Looking at the two different closed loop systems, it is clear that both controllers are successful in getting the state  $x_t$  close to zero by six time steps. However, it is not clear whether one system performs better than the other.



(a) Oscillating state and control profiles.

(b) Smooth but slower control and state profiles.

Figure 3.2: Two different control strategies  $u_t$  that lead to very different system responses  $x_t$ . Which one is better?

The state response shown in Figure 3.2a is somewhat oscillating, while the response in Figure 3.2b is smoother. If we have a case where the plant we wish to control does not operate safely whenever the state  $x_t$  is outside the region  $[-1, 1]$ , the first response is the better one since the state reaches the desired region at  $t = 1$ , i.e.,  $x_t \in [-1, 1] \forall t \geq 1$ , while the state response in Figure 3.2b is slower in reaching the desired region  $[-1, 1]$ . On the other hand, if an overshoot like the one in Figure 3.2a is unacceptable, the state behavior in Figure 3.2b is the better one out of the two.

If we have no concern for neither a safe region nor overshoots, but simply want the state  $x_t$  to be close to the reference point (zero), we can compare the two responses by evaluating the state's deviation from its reference. The most common way of comparing two state trajectories like the ones shown

<sup>5</sup>A SISO system is a Single Input Single Output system. It has one input ( $n_u = 1$ ) and one output, which in this subsection is the state variable. As discussed earlier the output may also be an auxiliary variable, e.g.,  $\gamma_t = Hx_t$ , instead of the states.

in Figure 3.2 is to compare a norm function of the form

$$\sum_{t=0}^N \|x_t - x_t^{\text{ref}}\|^2 \quad (3.12)$$

evaluated for each of the two trajectories. Here,  $N$  is the final time of interest (6 in our example). Sometimes the sum starts at  $t = 1$  instead of  $t = 0$ ; this is because the initial  $x_0$  is given and can therefore be left out since it contributes the same amount regardless of trajectory. Instead of letting the sum over  $x_t$  go from  $t = 1$  to  $t = N$ , we can take the sum over  $x_{t+1}$  from  $t = 0$  to  $t = N - 1$ . That is,

$$\sum_{t=1}^N \|x_t - x_t^{\text{ref}}\|^2 = \sum_{t=0}^{N-1} \|x_{t+1} - x_{t+1}^{\text{ref}}\|^2 \quad (3.13)$$

The relevance of this indexing convention will be apparent later.

Since  $x_t^{\text{ref}} \equiv 0$ , we compare

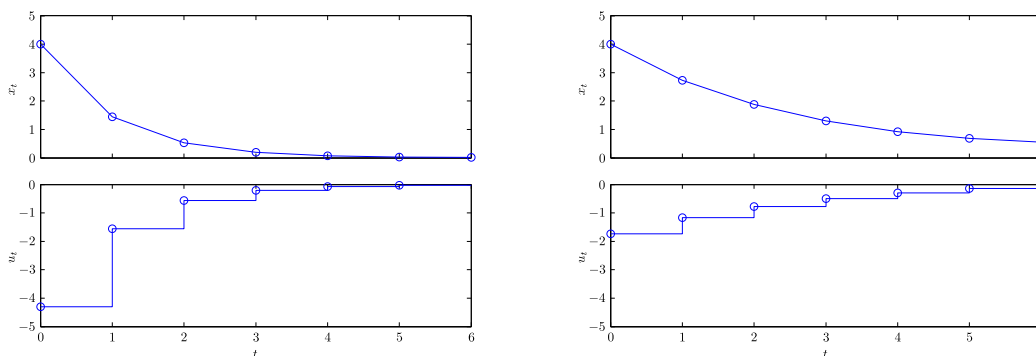
$$\sum_{t=0}^{6-1} \|x_{t+1}\|^2 \quad (3.14)$$

for the two cases. In (3.12), we implicitly assume that we use the 2-norm (Euclidean norm) which is by far the most common choice of norm. Nevertheless, we may in certain application use other norms such as 1-norm or  $\infty$ -norm. Calculating the performance measure (3.14) yields

$$\sum_{t=0}^{6-1} \|x_{t+1}\|_2^2 = \sum_{t=0}^5 x_{t+1}^2 = x_1^2 + x_2^2 + x_3^2 + x_4^2 + x_5^2 + x_6^2 \quad (3.15)$$

for each of our example responses in Figure 3.2 we get 0.9 for the oscillating state trajectory in Figure 3.2a and 2.4 for the smoother state trajectory in Figure 3.2b. Hence, if our goal is to have the state close 0 as measured by the 2-norm squared, the oscillating trajectory in Figure 3.2a is best.

The above discussion shows that there is no single answer to the question of which trajectory is best. Determining the best trajectory is only meaningful with respect to a measure of performance — no trajectory can be universally best or optimal. When discussing optimality in control we need to decide on a performance measure (an objective function) and compare trajectories based on that. The trajectory that is optimal with respect to one objective function may not be optimal with respect to another. In the following we will discuss several possible objective functions for control and provide some reasons for the most common choice of objective.



(a) Identical response to that of Figure 3.2b.

(b) The state approaches zero slower due to less control usage.

Figure 3.3: Another pair of different control strategies  $u_t$  that lead to different system responses  $x_t$ . Which one is better?

If we compare the two state trajectories in Figure 3.3, many would say that one in Figure 3.3a (the one where the state goes to zero fastest) is the best one. This is certainly true if we use an objective function like (3.12). However, we can imagine a system where it is potentially bad if the state is moved too quickly, for instance if rapid changes may cause damage; in a case like that the state trajectory in Figure 3.3b may be the best. If we want to include the control input as part of our performance measure or objective function, we might have more reasons to argue that the system behavior in Figure 3.3b is the one we prefer out of the two. Think of cases where the use of input  $u_t$  has a high cost associated with it; two examples are vehicles that run on expensive jet fuel and circuits powered by small batteries. In such cases we may want the state to approach its reference as fast as possible, but the cost associated with the use of input might be more important to us.

Looking at the two control input sequences  $u_t$  in Figure 3.3, it is clear that the control input in Figure 3.3a works the hardest (“spends the most fuel”). Since we want a systematic way of comparing control input sequences, we also here need a measure of performance. Again, there are many possible choices, but we will for now use a quadratic measure and discuss alternatives later. In fact, the measure we will use is almost identical to the one we used for the state trajectories:

$$\sum_{t=0}^{N-1} \|u_t\|^2 \quad (3.16)$$

Note that it is possible to include a reference input  $u_t^{\text{ref}}$  that we want to stay

close to, just like in (3.12)<sup>6</sup>. If we compare (3.14) and (3.16) we see that the sums go to  $t = N$  and  $t = N - 1$ , respectively. This is due to the fact that the last state we include in our performance measure is  $x_N$ , which depends on  $u_{N-1}$  since the discrete-time dynamic systems we study can be written as

$$x_{t+1} = g(x_t, u_t) \quad (3.17)$$

Hence, the control  $u_N$  affects the state  $x_{N+1}$ , a quantity we are not interested in (since it does not appear in the sum in (3.14)). Evaluating the control performance measure

$$\sum_{t=0}^5 \|u_t\|_2^2 = \sum_{t=0}^5 u_t^2 = u_0^2 + u_1^2 + u_2^2 + u_3^2 + u_4^2 + u_5^2 \quad (3.18)$$

for the two input sequences in Figures 3.3a and 3.3b results in 21.3 and 5.3, respectively. These numbers quantify the amount of work done by each of the controllers and confirm that the controller in Figure 3.3a works more than the other.

We now have a way of evaluating how well a dynamic system performs, both in terms of how much the state deviates from its reference point and how much work the controller does to achieve this. Both of these quantities should be as small as possible — we want to minimize them. When the two quantities are minimized we get a state trajectory that stays close to its reference and a controller that achieves this with a small amount of work.

The task of determining the best performance gets more complicated when we simultaneously consider both state and control trajectories. The answer to which of the dynamic systems in Figure 3.3 has the best performance depends whether we prioritize the state being close to its reference or a small input signal. We can argue that Figure 3.3a performs best if one mainly cares about how close the state is to its reference, and that Figure 3.3b is best if how much input is being used is our main concern.

Let us consider combining the two performance measures (one for the state and one for the control input) into one objective function  $f$  by adding them together:

$$\begin{aligned} f &= \sum_{t=0}^{N-1} x_{t+1}^2 + \sum_{t=0}^{N-1} u_t^2 \\ &= \sum_{t=0}^{N-1} x_{t+1}^2 + u_t^2 \end{aligned} \quad (3.19)$$

---

<sup>6</sup>The use of the reference control input  $u^{\text{ref}}$  is also mentioned in Section 4.2.4.

This objective function takes both state error and control usage into account. However, it does not allow us to place any emphasis on what is most important to us — control design. We can specify our priority by introducing the *weight parameters*  $q$  and  $r$  and use an objective function of the form

$$f = \sum_{t=0}^{N-1} qx_{t+1}^2 + ru_t^2 \quad (3.20)$$

The (positive) weights  $q$  and  $r$  are chosen by the control designer as a way to specify the desired system behavior and tune controller. In cases where a small state error is more important than low use of control input we make sure that  $q$  is large enough relative to  $r$ ; similarly, when minimizing control input usage takes precedence over keeping the state close to its reference we increase  $r$  and/or decrease  $q$  until we are happy with the overall performance. An example will clarify the effect of the weights.

**Example 3** (Different objective function values)

We consider the simple example system

$$x_{t+1} = 0.9x_t + 0.5u_t \quad (3.21)$$

with initial condition  $x_0 = 4$ . As above, we want to control the state  $x_t$  to 0 without using too much input  $u$ , and we still study  $N = 6$  time steps. First, assume that it is very important that the state reaches 0 quickly and stays very close, and that we do not worry much about how much control input we use. We can specify this by choosing a value of  $q$  that is large relative to the value of  $r$ . We choose  $q = 5$  and  $r = 1$  and see if the system behavior that minimizes the resulting objective function is acceptable. The optimal system response with respect to this choice of weights is shown in Figure 3.4. We see that the state fairly quickly goes to 0, and that there is a fairly liberal use of control input to achieve this, especially for the first few time steps. We can quantify the performance through

$$\sum_{t=0}^{N-1} x_{t+1}^2 = 1.9, \quad \sum_{t=0}^{N-1} u_t^2 = 23.6 \quad (3.22)$$

If we decide that in Figure 3.4 the state goes to 0 faster than strictly necessary, or that the large values of the input is not worth the quick state response, we can reconsider our choices of  $q$  and  $r$ . That is, we want to put less emphasis on the state's quick convergence to 0. We can specify this by decreasing  $q$ , increasing  $r$ , or both. For simplicity, we just decrease  $q$  to  $q = 2$



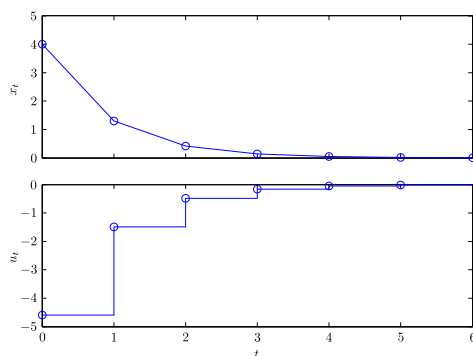


Figure 3.4: Optimal system behavior with respect to the weights  $q = 5$  and  $r = 1$ .

and leave  $r = 1$ . The response shown in Figure 3.5 is optimal with respect to the objective function (3.20) with  $q = 2$  and  $r = 1$ . If we compare this response with the one shown in Figure 3.4 that resulted from  $q = 5$ , we see that the state now approaches 0 slower (it is very close to 0 at  $t = 6$ ) and that the magnitude of the control input is smaller. This is also seen through the quantities

$$\sum_{t=0}^{N-1} x_{t+1}^2 = 4.8, \quad \sum_{t=0}^{N-1} u_t^2 = 14.7 \quad (3.23)$$

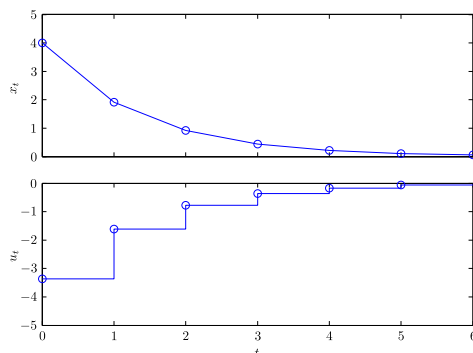


Figure 3.5: Optimal system behavior with respect to the weights  $q = 2$  and  $r = 1$ .

Let us assume that we have changed our minds, and now put even less emphasis on how quick the state goes to 0, as long as it is decreasing, and put a bigger emphasis on how much control input is used. This can be expressed through the choice  $q = 1$  and  $r = 2$ . The system behavior shown in Figure 3.6 is optimal with respect to this choice. The state is no longer close to 0 by

$t = 6$ , but the control usage now has a very small magnitude; specifically,

$$\sum_{t=0}^{N-1} x_{t+1}^2 = 14.3, \quad \sum_{t=0}^{N-1} u_t^2 = 5.3 \quad (3.24)$$

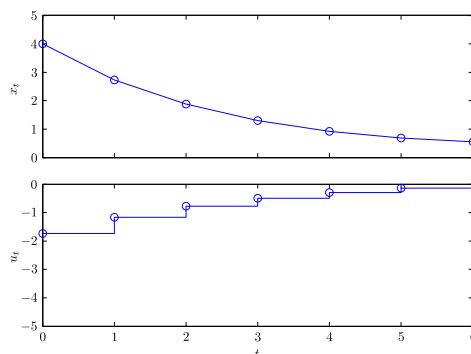


Figure 3.6: Optimal system behavior with respect to the weights  $q = 1$  and  $r = 2$ .

Note that no one out of these three system responses is better than the others — they are all optimal with respect to a specific choice of objective function weights. It is not always easy to predict what kind of response any given choice of  $q$  and  $r$  will produce, and it is often necessary to try many different combinations before a good combination is found.  $\triangle$

In the discussion above we measured control performance in terms of control *usage*, meaning we wanted to minimize the magnitude of the control signal. We mentioned a few examples where this makes sense, one being when the use of control input is directly related to consuming a resource, such as electricity from a battery or fuel. In many applications, a large control signal magnitude has no direct cost. Examples of such cases include the rudder angle of a ship and the valve opening in a pipe. In these examples we often want to minimize how much the control signal changes from one time step to the next, often due to the wear and tear associated with large and frequent changes in the actuator set point.

We define the change in input at time  $t$  as, cf. (3.8i),

$$\Delta u_t = u_t - u_{t-1} \quad (3.25)$$

which is simply the difference between the input at time  $t$  and the input at the previous time  $t - 1$ . The quantity  $\Delta u_t$  is as mentioned earlier referred to as a control move. If we want to limit how much the control input changes,

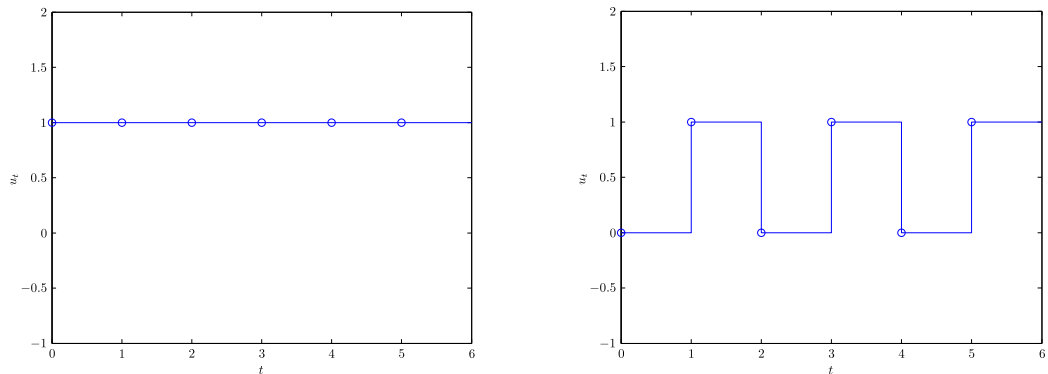
we may include this in the objective function we minimize. This is usually done by adding the square of the term (3.25) to the sum in the objective function (3.20), commonly with an associated (positive) weight that we will call  $r_\Delta$ <sup>7</sup>. This leads to the objective function<sup>8</sup>

$$f = \sum_{t=0}^{N-1} qx_{t+1}^2 + ru_t^2 + r_\Delta(\Delta u_t)^2 \quad (3.26)$$

As an exercise, find the value of

$$\sum_{t=0}^{N-1} r_\Delta(\Delta u_t)^2 \quad (3.27)$$

for each of the two input sequences in Figure 3.7 when  $r_\Delta = 1$ ,  $N = 6$ , and  $u_{-1} = 0$ . The answer can be found in the footnote.<sup>9</sup>



(a) A constant input sequence.

(b) An on-off input sequence.

Figure 3.7: Two different control input sequences.

As with the other terms in the objective function, we could have achieved reduction in the control moves in different ways. The approach we presented here is the most common in the literature, and using the square of the change in input from one time instant to the next is the most consistent with the rest of the objective function. Alternatives to this approach is beyond the scope of this text; furthermore, the main goal of this brief discussion of the topic is to demonstrate that the chosen approach makes sense and to help build some intuition for why it makes sense.

<sup>7</sup>The notation is consistent with (3.11).

<sup>8</sup>The ' $\frac{1}{2}$ ' term is skipped below.

<sup>9</sup>Answers to the exercise: The sum in (3.27) is 1 (not 0!) for the control input in Figure 3.7a. The sum in (3.27) is 5 for the control input in Figure 3.7b.

### 3.4.1 Norms in the objective function

All of our objective functions discussed here were based on the 2-norm. We mentioned above that other norms can be used but the 2-norm is by far the most common in optimal control. The 1-norm is used in certain applications, meaning performance is measured through absolute values, rather than squares. As we will see in the subsequent sections, optimizing the performance of linear systems using a quadratic objective function is done by formulating quadratic programming problems. If we instead use the 1-norm, the objective function is not quadratic and the resulting optimization problem is no longer a QP. In order to solve an optimization problem where the objective function is a sum of absolute values of the variables, and the constraints are linear, it is possible to reformulate the problem and obtain a linear programming problem. That is, using the 1-norm as a performance measure in optimal control of linear systems leads to linear programming problems. The technique used to reformulate a 1-norm objective function involves introducing extra variables, but the details of this is outside the scope of this text.

## 3.5 Optimal open loop optimization examples

We continue this section with two examples of open loop optimization problems. The first example uses a SISO system while the second discusses a *MIMO system*<sup>10</sup>.

**Example 4** (Finite horizon optimal open loop control for a SISO system)  
Consider the scalar dynamic discrete-time system

$$x_{t+1} = ax_t + bu_t \quad (3.28)$$

Our goal is to keep the state  $x_t$  as close to zero as possible while using a minimal amount of input. This can be formulated as minimizing some combination of  $qx_t^2$  and  $ru_t^2$  for all time instants  $t$ , where  $q$  and  $r$  are non-negative scalars that reflect how we prioritize the two objectives relative to each other. Assume we care more about keeping the state close to zero than about how much input we use; this would be the case if performance is critical and fuel is cheap. We could then choose values like

$$q = 4, \quad r = 1 \quad (3.29)$$

---

<sup>10</sup>A MIMO system is a Multiple Input Multiple Output system. Thus, it has more than one input ( $n_u > 1$ ) and more than one output.

for every value of  $t$  provided the values of  $x_t$  and  $u_t$  are similar<sup>11</sup>. If the time horizon for optimization is of length  $N$ , we can formulate the objective as minimization of

$$f(z) = \sum_{t=0}^{N-1} \frac{1}{2} q_{t+1} x_{t+1}^2 + \frac{1}{2} r_t u_t^2 \quad (3.30)$$

where

$$z = (x_1, \dots, x_N, u_0, \dots, u_{N-1})^\top \quad (3.31)$$

That is,  $z$  is a vector containing all variables. For the remainder of this example, we choose the rather short horizon length  $N = 4$ . We then have that

$$z = (x_1, x_2, x_3, x_4, u_0, u_1, u_2, u_3)^\top \quad (3.32)$$

With this definition of  $z$ , the objective function (3.30) can be written

$$f(z) = \frac{1}{2} z^\top \underbrace{\begin{bmatrix} q_1 & 0 & 0 & 0 & 0 & 0 & 0 & 0 \\ 0 & q_2 & 0 & 0 & 0 & 0 & 0 & 0 \\ 0 & 0 & q_3 & 0 & 0 & 0 & 0 & 0 \\ 0 & 0 & 0 & q_4 & 0 & 0 & 0 & 0 \\ 0 & 0 & 0 & 0 & r_1 & 0 & 0 & 0 \\ 0 & 0 & 0 & 0 & 0 & r_2 & 0 & 0 \\ 0 & 0 & 0 & 0 & 0 & 0 & r_3 & 0 \\ 0 & 0 & 0 & 0 & 0 & 0 & 0 & r_4 \end{bmatrix}}_G z \quad (3.33)$$

where we call the big matrix  $G$ . If we write out the quadratic form,

$$f(z) = \frac{1}{2} z^\top G z = \frac{1}{2} (q_1 x_1^2 + q_2 x_2^2 + q_3 x_3^2 + q_4 x_4^2 + r_0 u_0^2 + r_1 u_1^2 + r_2 u_2^2 + r_3 u_3^2) \quad (3.34)$$

it is clear that (3.30) and (3.33) are equivalent.

We now rewrite the state Equation (3.28) as

$$-ax_t + x_{t+1} - bu_t = 0 \quad (3.35)$$

With this formulation, we can write the state equation for each time instant  $t$ :

$$-ax_0 + x_1 - bu_0 = 0 \quad (3.36a)$$

$$-ax_1 + x_2 - bu_1 = 0 \quad (3.36b)$$

$$-ax_2 + x_3 - bu_2 = 0 \quad (3.36c)$$

$$-ax_3 + x_4 - bu_3 = 0 \quad (3.36d)$$

<sup>11</sup>Similar values for  $x_t$  and  $u_t$  are obtained by scaling these variables.

This set of the equations can then be written in this fashion.

$$\begin{array}{rccccccccc}
 x_1 & & & & & & -bu_0 & & & = & ax_0 \\
 -ax_1 & +x_2 & & & & & & & -bu_1 & = & 0 \\
 & -ax_2 & +x_3 & & & & & & & = & 0 \\
 & & -ax_3 & +x_4 & & & & & -bu_2 & = & 0 \\
 & & & & & & & & & -bu_3 = & 0
 \end{array}$$

This suggests the matrix formulation

$$\underbrace{\begin{bmatrix} 1 & 0 & 0 & 0 & -b & 0 & 0 & 0 \\ -a & 1 & 0 & 0 & 0 & -b & 0 & 0 \\ 0 & -a & 1 & 0 & 0 & 0 & -b & 0 \\ 0 & 0 & -a & 1 & 0 & 0 & 0 & -b \end{bmatrix}}_{A_{\text{eq}}} \underbrace{\begin{bmatrix} x_1 \\ x_2 \\ x_3 \\ x_4 \\ u_0 \\ u_1 \\ u_2 \\ u_3 \end{bmatrix}}_z = \underbrace{\begin{bmatrix} ax_0 \\ 0 \\ 0 \\ 0 \end{bmatrix}}_{b_{\text{eq}}} \quad (3.37)$$

i.e., the set of system equations can be written as an equality constraint of the form

$$A_{\text{eq}}z = b_{\text{eq}} \quad (3.38)$$

Bounds on the states and controls are written

$$x^{\text{low}} \leq x_t \leq x^{\text{high}} \quad (3.39a)$$

$$u^{\text{low}} \leq u_t \leq u^{\text{high}} \quad (3.39b)$$

We can write these constraints in terms of  $z$  as

$$\begin{bmatrix} x_1 \\ x_2 \\ x_3 \\ x_4 \\ u_0 \\ u_1 \\ u_2 \\ u_3 \end{bmatrix} \geq \begin{bmatrix} x^{\text{low}} \\ x^{\text{low}} \\ x^{\text{low}} \\ x^{\text{low}} \\ u^{\text{low}} \\ u^{\text{low}} \\ u^{\text{low}} \\ u^{\text{low}} \end{bmatrix}, \quad - \begin{bmatrix} x_1 \\ x_2 \\ x_3 \\ x_4 \\ u_0 \\ u_1 \\ u_2 \\ u_3 \end{bmatrix} \geq - \begin{bmatrix} x^{\text{high}} \\ x^{\text{high}} \\ x^{\text{high}} \\ x^{\text{high}} \\ u^{\text{high}} \\ u^{\text{high}} \\ u^{\text{high}} \\ u^{\text{high}} \end{bmatrix} \quad (3.40)$$

The problem is fairly easy to implement and solve in MATLAB using this formulation. For simplicity we let the system be stable and choose  $a = 0.9$  and  $b = 0.5$ ; we also set  $x_0 = 4$ ,  $x^{\text{low}} = -10$ ,  $x^{\text{high}} = 10$ ,  $u^{\text{low}} = -2$ ,  $u^{\text{high}} = 2$ , as well as the tuning parameters  $q = 4$  and  $r = 1$  for all  $t$ . The resulting optimal open loop state and control sequences are shown in Figure 3.8. Note that the first two control inputs are at the lower bound, and that the state does not reach zero at the end of the horizon.  $\triangle$

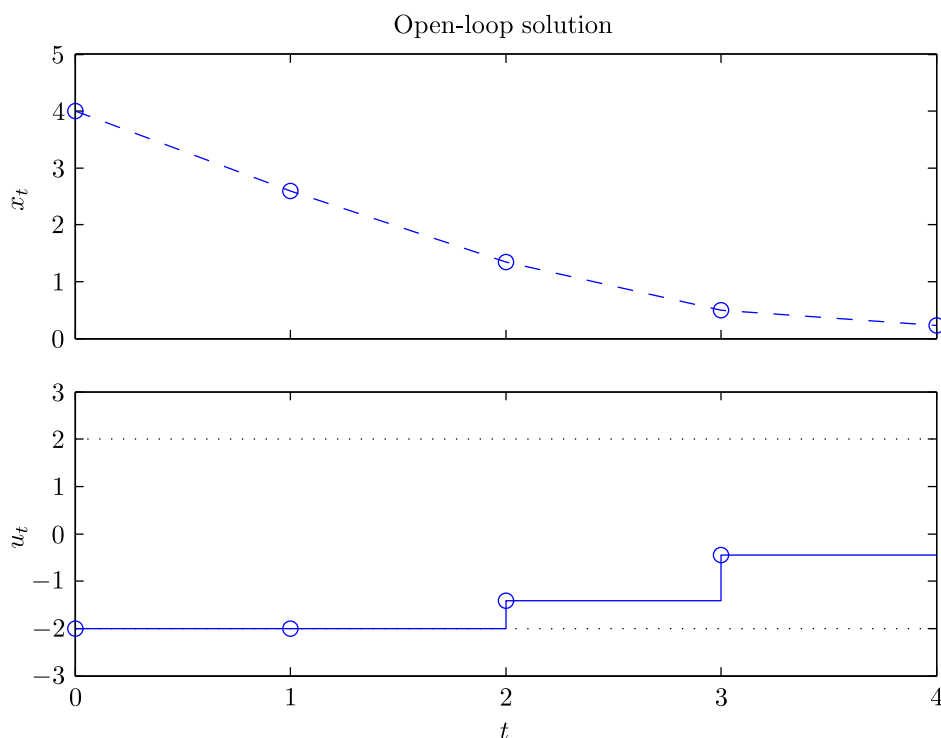


Figure 3.8: Open loop optimal state trajectory and control sequence for Example 4.

The next example is more general than the previous one, and extends the formulation to MIMO systems.

**Example 5** (Finite horizon optimal open loop control for a MIMO system) Consider the MIMO system

$$x_{t+1} = A_t x_t + B_t u_t \quad (3.41)$$

where  $x_t \in \mathbb{R}^2$  and  $u_t \in \mathbb{R}^2$ . Again, we wish to keep both states at zero with minimal use of input. This can be formulated as minimizing some combination of  $x_t^\top Q x_t$  and  $u_t^\top R u_t$  for all time instants  $t$ , where  $Q$  and  $R$  are matrices that reflect how we prioritize the different objectives relative to each other. We have here assumed that  $Q$  and  $R$  do not vary with time. If there are two states and two control inputs and we for instance care more about keeping the first state of  $x_t$  small than we care about keeping the second state of  $x_t$  small, we could use

$$Q = \begin{bmatrix} 2 & 0 \\ 0 & 1 \end{bmatrix} \quad (3.42a)$$





For some arbitrary horizon length  $N$ , we can write the state equations as the equality constraint  $A_{\text{eq}}z = b_{\text{eq}}$  with

$$A_{\text{eq}} = \left[ \begin{array}{cccc|cccc} I & 0 & \cdots & \cdots & 0 & -B_0 & 0 & \cdots & \cdots & 0 \\ -A_1 & I & \ddots & & \vdots & 0 & \ddots & \ddots & & \vdots \\ 0 & \ddots & \ddots & \ddots & \vdots & \vdots & \ddots & \ddots & \ddots & \vdots \\ \vdots & \ddots & \ddots & \ddots & 0 & \vdots & & \ddots & \ddots & 0 \\ 0 & \cdots & 0 & -A_N & I & 0 & \cdots & \cdots & 0 & -B_N \end{array} \right] \quad (3.49a)$$

and

$$b_{\text{eq}} = \begin{bmatrix} A_0 x_0 \\ 0 \\ \vdots \\ 0 \end{bmatrix} \quad (3.49b)$$

For our short horizon ( $N = 2$ ), we then get

$$A_{\text{eq}} = \left[ \begin{array}{cc|cc} I & 0 & -B_0 & 0 \\ -A_1 & I & 0 & -B_1 \end{array} \right], \quad \text{and} \quad b_{\text{eq}} = \begin{bmatrix} A_0 x_0 \\ 0 \end{bmatrix} \quad (3.50)$$

Regardless of the number of states, control inputs, and the horizon length, this formulation is fairly simple to implement in MATLAB.  $\triangle$

### 3.6 Dynamic optimization with nonlinear discrete time models

In Section 3.3 the system dynamics were given by a linear dynamic model. Now a nonlinear dynamic model is introduced. This changes (3.8) to

$$\min_{z \in \mathbb{R}^n} f(z) = \sum_{t=0}^{N-1} \frac{1}{2} x_{t+1}^\top Q_t x_{t+1} + d_{xt+1}^\top x_t + \frac{1}{2} u_t^\top R_t u_t + d_{ut}^\top u_t \quad (3.51a)$$

subject to

$$x_{t+1} = g(x_t, u_t) \quad (3.51b)$$

$$x_0, u_{-1} = \text{given} \quad (3.51c)$$

$$x^{\text{low}} \leq x_t \leq x^{\text{high}} \quad (3.51d)$$

$$u^{\text{low}} \leq u_t \leq u^{\text{high}} \quad (3.51e)$$

$$-\Delta u^{\text{high}} \leq \Delta u_t \leq \Delta u^{\text{high}} \quad (3.51f)$$

$$Q_t \succeq 0 \quad (3.51g)$$

$$R_t \succeq 0 \quad (3.51h)$$

The comments that apply to (3.8) and were discussed above are equally relevant in this case. There is however one key difference and that is the nonlinear discrete time model which introduces nonlinear equality constraints. Hence, (3.8) is an NLP problem and thus also a nonconvex problem. This complicates matters since solution methods require much more runtime. Further, solution methods are less robust in the sense that a solution, if it exists, may not be found, and finally, there are few ways to determine the quality of a solution<sup>12</sup>.

An NLP solver is needed to solve (3.51). There are two main classes of solver, *sequential quadratic programming (SQP)* and *interior point methods* as discussed in Chapter 18 and 19 in Nocedal and Wright (2006), respectively.

From a control viewpoint the future state trajectory  $x_1, \dots, x_N$  is given by the initial state  $x_0$  and the control trajectory  $u_0, \dots, u_{N-1}$  through the nonlinear discrete time model. Therefore the states may be eliminated by substituting  $x_0, \dots, x_N$  in the objective function and the state constraints with  $u_0, \dots, u_{N-1}$  using (3.51b) and (3.51c). As in the linear case this reduces the number of decision variables significantly when  $n_x \gg n_u$ . There is, however, an additional penalty to be paid in the nonlinear case. The linear state constraints (3.51d) are nonlinear in the control inputs. As an example the state constraints at  $t = 1$

$$x^{\text{low}} \leq x_1 \leq x^{\text{high}}$$

change to two nonlinear constraints in  $u_0$ . (Remember that  $x_0$  is fixed.)

$$x^{\text{low}} \leq g(x_0, u_0) \leq x^{\text{high}}$$

Problem (3.51) may be generalized by using  $f_t(x_t, u_t)$  instead of the quadratic term  $x_t^\top Q_t x_t + d_{xt} x_t + u_t^\top R_t u_t + d_{ut} u_t$ . As argued above the quadratic term covers most practical cases. Further, for linear models,  $f_t(x_t, u_t)$  transform a convex QP problem, or an LP problem<sup>13</sup>, into an NLP problem. Thus,

<sup>12</sup>The quality of a solution may for instance be measured by the duality gap.

<sup>13</sup>If  $Q_t = 0$  and  $R_t = 0$ .

this enforces a heavy penalty in terms of runtime and reliability. For non-linear models the penalty by introducing  $f_t(x_t, u_t)$  instead of the quadratic term will be less since (3.51) is an NLP problem in the first place.

# Chapter 4

## Optimal control

In this chapter we attempt to bridge the gap between dynamic optimization and control. This will be done by first presenting a concept which merges feedback control with dynamic optimization; *Model Predictive Control (MPC)*. Second, *linear MPC* in which a convex QP problem is the core component is reviewed. Third, the linear MPC problem is relaxed by removing inequality constraints. This is known as the *linear quadratic (LQ)* controller where the solution is given by a linear controller. Fourth, *nonlinear MPC (NMPC)*, which uses a nonlinear dynamic model, is briefly treated before this section ends with some additional comments.

### 4.1 Model predictive control

In Sections 3.3 and 3.6 we presented dynamic optimization where a discrete time model is optimized on a time horizon from  $t = 0$  to  $t = N$ . This is an *open loop optimization problem* since there is no feedback present in the solution. In other words the solution is computed at time  $t = 0$  and this solution is used throughout the prediction horizon. There is an alternative to this, *closed loop optimization*, in which the optimal solution is recomputed at every time step  $t$  to include feedback control. Mayne et al. (2000) formulate the MPC principle as

Model predictive control is a form of control in which the current control action is obtained by solving, at *each* sampling instant, a finite horizon open loop optimal control problem, using the current state of the plant as the initial state; the optimization yields an optimal control sequence and the first control in this sequence is applied to the plant.

---

**Algorithm 2** State feedback MPC procedure
 

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```

for  $t = 0, 1, 2, \dots$  do
  Get the current state  $x_t$ .
  Solve a dynamic optimization problem on the prediction horizon from  $t$ 
  to  $t + N$  with  $x_t$  as the initial condition.
  Apply the first control move  $u_t$  from the solution above.
end for

```

---

A basic MPC algorithm is given below.

The dynamic optimization problem referenced in the algorithm may be the convex QP problem (3.8) or the nonconvex NLP problem (3.51).

One remark is in order. We will always assume that the constraints, which in (3.8) and (3.51) are defined on the time intervals  $0, \dots, N-1$  and  $1, \dots, N$ , are aligned with  $t$  meaning that they are shifted to  $t, \dots, t + N - 1$  and  $t + 1, \dots, t + N$  at time  $t$ .

The concept is illustrated in Fig. 4.1 and it essentially solves a similar optimization problem over and over again at each time step. Hence, MPC uses a *moving horizon*<sup>1</sup> approach in which the prediction horizon changes from  $t, \dots, t + N$  to  $t + 1, \dots, t + N + 1$  from one time step to the next.

One obvious question is “What is the advantage of MPC vs. the open loop solution?” The brief answer is that *MPC couples open loop optimization with feedback control* in the following way: At each time step MPC requires a new solution of the dynamic optimization problem. This solution  $z_t^*$  contains the future states  $x_{t+1}^*, \dots, x_{t+N}^*$ . Recalling (3.8c) or (3.51c) the optimization problem at  $t + 1$  requires an initial value, i.e.,  $x_{t+1}$ . A key question is how to select this initial value. One option is to use the prediction  $x_{t+1}^*$  computed at  $t$ . However, this prediction does not account for errors in the discrete time model and disturbances that occur on the time interval between  $t$  and  $t + 1$ . Hence, a better option is to compute a state estimate  $\hat{x}_{t+1}$  which relies on the latest available measurements and use this instead of  $x_{t+1}^*$ . State estimation extends Algorithm 2 as follows.

Before moving on we reiterate on the difference between Algorithm 2 and Algorithm 3. Algorithm 2 requires an exact measure of the state at each time step and is for this reason called *state feedback MPC*. Algorithm 3 relies on a state estimate which uses available measurements, i.e., available output data, and is for this reason denoted *output feedback MPC*.

To clarify, the term measured data in Algorithm 3 includes both the control input  $u_t$  and the measured output. The latter will be defined in

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<sup>1</sup>The name receding horizon is also used.

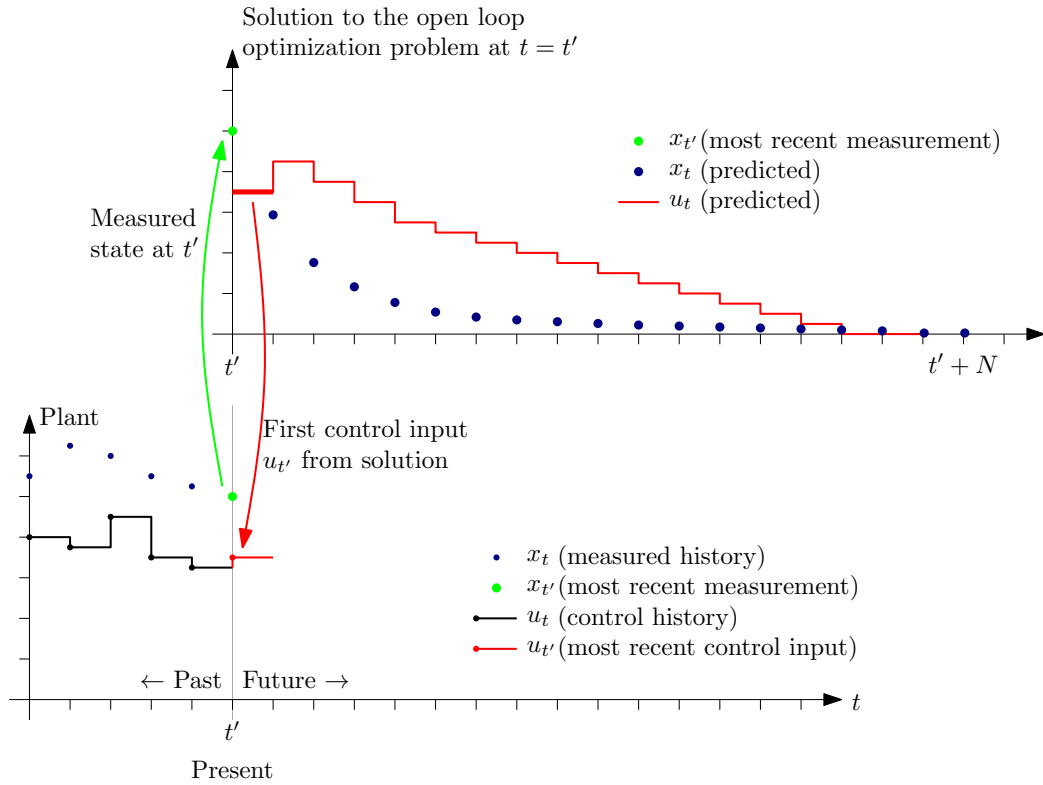


Figure 4.1: Illustration of the MPC principle.

---

**Algorithm 3** Output feedback MPC procedure
 

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**for**  $t = 0, 1, 2, \dots$  **do**

    Compute an estimate of the current state  $\hat{x}_t$  based on the measured data up until time  $t$ .

    Solve a dynamic optimization problem on the prediction horizon from  $t$  to  $t + N$  with  $\hat{x}_t$  as the initial condition.

    Apply the first control move  $u_t$  from the solution above.

**end for**

---

conjunction with state estimation (4.9).

Several books are available on MPC. Arguably the most comprehensive reference is Rawlings and Mayne (2009)<sup>2</sup>.

## 4.2 Linear MPC

Linear MPC applies the MPC concept to problems with quadratic objective functions and linear constraints. Hence, a convex QP problem, like (3.8), is solved at each time step. We make two changes to this QP problem before stating the algorithm. First, it runs for all times, i.e.,  $t = 0, 1, \dots$ , and second, it includes control input changes, i.e.,  $\Delta u_t$ , in the objective function since this is common in MPC.

$$\begin{aligned} \min_{z \in \mathbb{R}^n} f(z) = & \sum_{t=0}^{N-1} \frac{1}{2} x_{t+1}^\top Q_{t+1} x_{t+1} + d_{xt+1} x_{t+1} \\ & + \frac{1}{2} u_t^\top R_t u_t + d_{ut} u_t + \frac{1}{2} \Delta u_t^\top R_{\Delta t} \Delta u_t \end{aligned} \quad (4.1a)$$

subject to

$$x_{t+1} = A_t x_t + B_t u_t \quad (4.1b)$$

$$x_0, u_{-1} = \text{given} \quad (4.1c)$$

$$x^{\text{low}} \leq x_t \leq x^{\text{high}} \quad (4.1d)$$

$$u^{\text{low}} \leq u_t \leq u^{\text{high}} \quad (4.1e)$$

$$-\Delta u^{\text{high}} \leq \Delta u_t \leq \Delta u^{\text{high}} \quad (4.1f)$$

where

$$Q_t \succeq 0 \quad (4.1g)$$

$$R_t \succeq 0 \quad (4.1h)$$

$$R_{\Delta t} \succeq 0 \quad (4.1i)$$

$z$  and  $\Delta u_t$  is defined as in (3.8).

The state feedback linear MPC algorithm is given by Algorithm 4.

We will now discuss this algorithm starting with a simple example, and address the non zero reference case as in (3.10) later.

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<sup>2</sup>This book is freely available for download at <http://www.nobhillpublishing.com>.

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**Algorithm 4** Linear MPC with state feedback
 

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**for**  $t = 0, 1, 2, \dots$  **do**

    Get the current state  $x_t$ .

    Solve the convex QP problem (3.8) on the prediction horizon from  $t$  to  $t + N$  with  $x_t$  as the initial condition.

    Apply the first control move  $u_t$  from the solution above.

**end for**

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**Example 6** (Comparing MPC with an open loop strategy)

Consider the unstable scalar system

$$x_{t+1} = ax_t + bu_t \quad (4.2)$$

with  $a = 1.2$ , and  $b = 0.5$ , and objective function

$$f(z) = \sum_{t=0}^{N-1} \frac{1}{2}qx_{t+1}^2 + \frac{1}{2}ru_t^2 \quad (4.3)$$

with  $N = 4$ ,  $q = 1$ , and  $r = 4$ . Figure 4.2 shows all open loop solutions with a prediction horizon length of  $N = 4$  in a simulation of 15 time instants. The open loop solution at  $t = 0$  is shown with one filled blue dot at  $t = 1$  and three unfilled blue dots at  $t = 2, 3, 4$ . The same holds for the control input. The same coloring scheme is repeated for each time step.  $\triangle$

There are some important observations to be made from this idealized example where the state is assumed to be known and where there are no model errors<sup>3</sup>, i.e., the model used in the MPC algorithm equals the model which drives the real system.

The open loop solution computed at  $t = 1$ , i.e., for  $t = 2, 3, 4, 5$ , clearly differs from the open loop solution calculated at  $t = 0$ , both for the state  $x_t$  and the control input  $u_t$ . This is seen by for instance comparing the filled and unfilled blue dots at  $t = 2$ . The same also holds for all later time steps. Hence, the open loop solution and the MPC solution, which are marked as filled dots, differ even in this case with no uncertainty in the discrete time model or noisy measurements.

### 4.2.1 Ensuring feasibility at all times

Returning to Algorithm 4 a relevant question is: “Will there always exist a feasible point?” The answer is clearly no and a simple example illustrates why.

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<sup>3</sup>Model errors occur when the actual system differs from the MPC model. This is always the case in a practical application.



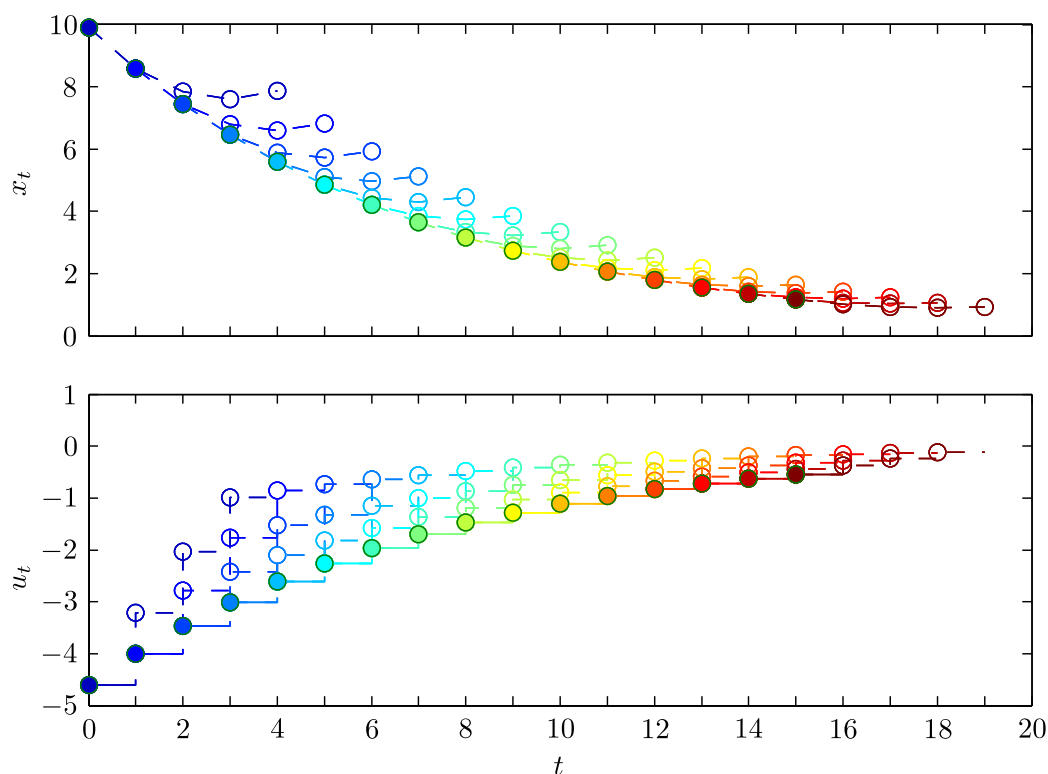


Figure 4.2: Simulation of the system (4.2) with MPC using the objective function (4.3).

**Example 7** (Infeasible solution)

Imagine a vehicle that moves along one axis and therefore has two states, position and velocity. It is controlled by Algorithm 4. Further, there are linear control input constraints as well as linear state constraints, which must be satisfied at each time step, see (4.1d) and (4.1e). The control input constraints could refer to a power limit while the state constraints may refer to limits in allowable vehicle position. Now, imagine a severe disturbance occurring between time step  $t - 1$  and  $t$ , which moves the vehicle beyond the state constraint limits. In this case no feasible point may exist at  $t$  since the state constraints at  $t + 1$ , and possibly at consecutive time steps, may be violated for all feasible control inputs.  $\triangle$

The example shows that a feasible point may not exist and that a control input may not be available. This is an unacceptable situation. To avoid this we soften the state constraints in (4.1) by using *slack variables*. This is shown below where the time index  $t$  runs indefinitely as in Algorithm 4.

$$\begin{aligned} \min_{z \in \mathbb{R}^n} f(z) = & \sum_{t=0}^{N-1} \frac{1}{2} x_{t+1}^\top Q_t x_{t+1} + d_{xt+1}^\top x_{t+1} + \frac{1}{2} u_t^\top R_t u_t + d_{ut}^\top u_t \\ & + \frac{1}{2} \Delta u_t^\top R_{\Delta t} u_t + \rho^\top \epsilon + \frac{1}{2} \epsilon^\top S \epsilon \end{aligned} \quad (4.4a)$$

subject to

$$x_{t+1} = A_t x_t + B_t u_t \quad (4.4b)$$

$$x_0, u_{-1} = \text{given} \quad (4.4c)$$

$$x^{\text{low}} - \epsilon \leq x_t \leq x^{\text{high}} + \epsilon \quad (4.4d)$$

$$u^{\text{low}} \leq u_t \leq u^{\text{high}} \quad (4.4e)$$

$$-\Delta u^{\text{high}} \leq \Delta u_t \leq \Delta u^{\text{high}} \quad (4.4f)$$

where

$$\epsilon \in \mathbb{R}^{n_x} \geq 0$$

$$\rho \in \mathbb{R}^{n_x} \geq 0$$

$$S \in \text{diag} \{s_1, \dots, s_{n_x}\}, \quad s_i \geq 0, \quad i = \{1, \dots, n_x\}$$

The slack variable  $\epsilon$  and the tuning parameters  $\rho$  and  $s_1, \dots, s_{n_x}$  are defined such that all their elements are positive. Two terms have been added to the original QP problem,  $\rho^\top \epsilon$  and  $\frac{1}{2} \epsilon^\top S \epsilon$ . These are both positive terms, hence there is a desire to drive these terms to zero. More precisely the slack variables should be nonzero only if the corresponding constraints are violated. This corresponds to the definition of an *exact penalty function* in Chapter 15.4 in Nocedal and Wright (2006). The function (4.4) will be an exact penalty function in this sense provided the  $\rho$  elements are big enough. Again referring to Chapter 15.4 in Nocedal and Wright (2006) the quadratic term  $\frac{1}{2} \epsilon^\top S \epsilon$  alone can never guarantee an exact penalty function, no matter how large the elements  $s_1, \dots, s_{n_x}$  are. In practice an application will either use the linear term or the quadratic term.

The slack variable  $\epsilon$  may be time dependent by for instance selecting different variables for the first part of the horizon and the latter part, respectively. The reason is to prevent unnecessary constraint violation during the latter prediction horizon since constraint violation tends to appear early on the prediction horizon. Such an approach increases the number of slack variables and hence computation time.

The output constraints may be widened during the first time steps of the prediction horizon, or remove these output constraints altogether, in order to limit the use of slack variables.

## 4.2.2 Stability of linear MPC

A second relevant question for Algorithm 4 is: “Will the linear MPC controller always be stable?”, or which assumptions must be made in order to guarantee stability<sup>4</sup> of linear state feedback MPC? The somewhat surprising answer is that stability cannot be guaranteed even if a feasible solution exists for all  $t = 0, 1, \dots$ . A simple example illustrates this.

### Example 8 (Stability of linear MPC)

Assume the following objective function

$$f(x_1, u_0) = \frac{1}{2}(x_1^2 + ru_0^2), \quad r > 0 \quad (4.5a)$$

subject to

$$x_{t+1} = 1.2x_t + u_t \quad (4.5b)$$

$$x_0 = 1 \quad (4.5c)$$

There are no inequality constraints and the optimal control input at any time step  $t$ , i.e.,  $u_t$ , can therefore be written as an explicit function of  $x_t$  as follows:

$$u_t = -\frac{1.2}{r+1}x_t \quad (4.5d)$$

By inserting (4.5d) into (4.5b) we obtain the closed loop system dynamics.

$$x_{t+1} = \left(1.2 - \frac{1.2}{r+1}\right)x_t = \alpha x_t \quad (4.6)$$

The open loop system (4.5b) has an eigenvalue 1.2 and is therefore an open loop unstable system. The closed loop eigenvalue in (4.6) exceeds 1, i.e.,  $\alpha > 1$ , if  $r < 5$ , meaning that the closed loop system is unstable for these choices of  $r$ .  $\triangle$

This simple example illustrates the fact that an MPC controller may give rise to an unstable closed loop system, even though a feasible point exists at every time step. This rather confusing fact was an important reason why stability analysis of MPC lagged behind practical applications for many years. Early references of practical MPC applications dates back to the late 70’s and early 80’s, see e.g. Richalet et al. (1978) and Cutler and Ramaker (1980), while the first sound stability proof was published in the early 90’s. An excellent review of these topics is given in Rawlings and Muske (1993).

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<sup>4</sup>By stability we mean asymptotic stability, see e.g., Khalil (2002)

It is beyond the scope of this note to discuss stability in detail. We will however include some theoretical as well as practical comments.

The example above shows that feasibility of MPC is no guarantee for closed loop stability. Stability can, however, be proven by reformulating the MPC problem. There are several approaches. We will discuss a reformulation where the following equality constraint is added to (4.1):

$$x_N = 0 \tag{4.7}$$

In this case Algorithm 4 gives a stable closed loop solution provided a feasible solution is available at all times and that there are no model errors. Since there are no model errors, i.e., the MPC model and the actual system are identical, this is a *nominal stability* result. Adding (4.7), however, may cause infeasibility problems, in particular for short prediction horizons. An alternative to (4.7) is to increase the weight on the final state constraint, i.e.,  $Q_N$ , which has a similar effect to the equality constraint  $x_N = 0$ . We refer to Rawlings and Mayne (2009) for more theory on stability of linear MPC with state feedback. If we use Algorithm 4 with output feedback instead of state feedback, stability proofs are very involved and of limited use for practical algorithms. The key problem comes from the interaction between the dynamics of the estimation loop and the control loop. Some results are available, see e.g., Inslan et al. (2003). We will return with some comments on stability analysis in the later Section 4.4.3.

If we return to Example 8 stability is easily achieved by increasing the prediction horizon. As a general rule the prediction horizon must be at least as long as the *dominant dynamics*<sup>5</sup> <sup>6</sup>. In practice stability is no major issue provided the MPC controller is designed and tuned according to sound principles. This includes the choice of model and the length of prediction horizon. In addition MPC is seldom used to control unstable processes as will be discussed later.

### 4.2.3 Output feedback

As discussed several times state feedback is no realistic option. Output feedback is needed meaning that Algorithm 4 changes to Algorithm 5.

The state estimate  $\hat{x}_t$  is needed. In linear MPC different estimators are used depending on the model type. Since we focus on state space models there

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<sup>5</sup>The dominant dynamics is a qualitative term, which may be defined by the longest time constant of a stable system.

<sup>6</sup>Example 8 is an unstable system. In this case the time constant is not defined. However, the unstable eigenvalue gives an indication of the minimum prediction horizon, which in this case is about 5 time steps.

---

**Algorithm 5** Linear MPC with output feedback
 

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**for**  $t = 0, 1, 2, \dots$  **do**

    Compute an estimate of the current state  $\hat{x}_t$  based on the measured data up until time  $t$ .

    Solve the convex QP problem (3.8) on the prediction horizon from  $t$  to  $t + N$  with  $\hat{x}_t$  as the initial condition.

    Apply the first control move  $u_t$  from the solution above.

**end for**

---

are two main estimator classes, *Kalman filter based estimators* and *Moving horizon estimators (MHE)*. The celebrated Kalman filter was first proposed by Kalman (1960) and has been widely used since.

The structure of output feedback linear MPC is shown in Figure 4.3 and the estimator equations are given by

$$\hat{x}_{t+1} = A\hat{x}_t + Bu_t + K_F(y_t - \hat{y}_t) \quad (4.8a)$$

$$\hat{y}_t = C\hat{x}_t \quad (4.8b)$$

$$\hat{x}_0 = \text{given} \quad (4.8c)$$

where  $K_F$  is the *Kalman gain* and  $C$  is the *measurement matrix*, i.e., data  $y_t$  is measured at each sample. We assume a linear measurement model

$$y_t = Cx_t \quad (4.9)$$

The real system is defined within the dashed lines marked “System” while the estimator is marked by the “Estimator” dashed lines. The estimator receives measurements  $y_t$  and control signals  $u_t$ , and computes estimated states  $\hat{x}_t$  that are used by the controller. The system in the figure is an LTI system. In the case of an LTV system the appropriate choice is a time varying Kalman gain<sup>7</sup>. The controller solves the convex QP problem (3.8).

Using a Kalman filter complicates tuning of the MPC controller since the Kalman filter itself needs tuning. A rule of thumb is to make the estimator dynamics significantly faster than the linear MPC feedback loop to limit interaction between the estimator and the control loop.

As a remark the Kalman filter is based on a stochastic model description by adding noise terms to the dynamic model equation as well as the

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<sup>7</sup>Even in the LTI case a time varying Kalman gain can be applied by using the finite horizon formulation instead of the infinite (stationary) Kalman filter solution. This is, however, rarely done.

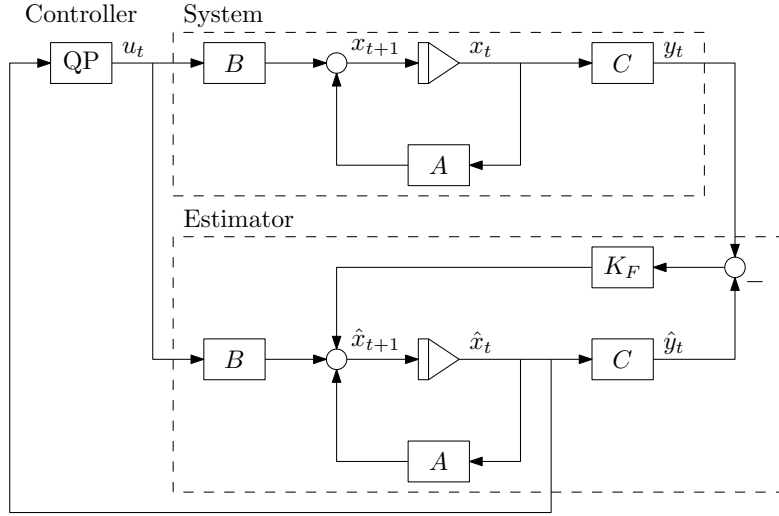


Figure 4.3: The structure of an output feedback linear MPC.

measurement model

$$x_{t+1} = Ax_t + Bu_t + v_t \quad (4.10a)$$

$$y_t = Cx_t + w_t \quad (4.10b)$$

where  $v_t$  and  $w_t$  are process noise and measurement noise terms, respectively, and the noise covariances of these terms determine the Kalman gain  $K_F$ . Hence, these covariances are used to tune the filter gain. If for instance the process noise covariance is much larger than the measurement noise covariance we rely a lot on the measurements, which in Kalman filter terms imply a large Kalman filter gain. In the opposite case the Kalman filter gain will be small. Kalman filter theory is described in many books, for instance in the comprehensive textbook Brown and Hwang (2012).

MHE is an estimator type that computes  $\hat{x}_t$  by solving an optimization problem (Rao et al., 2003). It uses recent data, i.e., data at times  $\{t - M, \dots, t\}$ , to estimate the current state  $x_t$ . Hence, MHE uses data on a time horizon backwards in time as opposed to MPC, which computes the control based on predictions forward in time. An advantage of MHE is that it easily accommodates state constraints. Examples of the latter are bounds on velocity, position, temperature and pressure. The MHE optimization problem is a convex QP problem in linear MPC. Hence, it can be solved by the same algorithm as the MPC problem.

### 4.2.4 Reference tracking and integral action

MPC should handle different types of control problems like disturbance rejection and setpoint tracking. The linear MPC formulation (4.1) may be regarded as a basic formulation and extensions are therefore needed to account for some control problems. In the following two key problems will be discussed; setpoint tracking and integral action.

A system may need to follow a reference trajectory, i.e., we may track some output variable, e.g., the position of a vessel or pressure in a reactor. This situation is covered by (4.1) as discussed in conjunction with (3.10)<sup>8</sup>. To be more explicit, however, assume that the goal is to track a variable  $\gamma_t$ , which depends linearly on the states, i.e.,  $\gamma_t = Hx_t$ .  $\gamma_t$  is usually called a controlled variable<sup>9</sup>. A suitable objective function, derived from (4.1), may be

$$f(z) = \sum_{t=0}^{N-1} \frac{1}{2} (\gamma_{t+1} - \gamma_{t+1}^{\text{ref}})^{\top} Q (\gamma_{t+1} - \gamma_{t+1}^{\text{ref}}) + \frac{1}{2} \Delta u_t^{\top} R_{\Delta} u_t \quad (4.11)$$

where  $Q \succeq 0$  and  $R \succ 0$ .

An important question is whether the reference trajectory is feasible. To simplify the discussion let us assume a fixed setpoint  $\gamma_t^{\text{ref}} = \gamma^{\text{ref}}$ , an LTI system and subsequently pose the question: Is the stationary point feasible? This can be analyzed as follows:

A stationary point  $(x^s, \gamma^s, u^s)$  is found by setting  $x_{t+1} = x_t$  in the system model.

$$\begin{aligned} x^s &= Ax^s + Bu^s \\ \gamma^s &= Hx^s \end{aligned}$$

Since the control input  $u_t$  is constrained by lower and upper bounds as in (4.1e), there may not exist a stationary state  $x^s$  such that  $\gamma^{\text{ref}} = \gamma^s$ . This can easily be checked since the model and constraints are all linear. A simple example illustrates this.

#### Example 9 (Feasibility of a stationary point)

<sup>8</sup>If  $d_{xt} = 0$  and  $d_{ut} = 0$  the origin is the optimal solution and hence the setpoint is 0 in this case.

<sup>9</sup>The term controlled variable, or CV, is discussed later in conjunction with practical aspects, see Section 4.6.5.

Assume the following stable linear system:

$$\begin{aligned} x_{t+1} &= \begin{bmatrix} 0.8 & 0.4 \\ -0.1 & 0.9 \end{bmatrix} x_t + \begin{bmatrix} 1.0 & 0.5 \\ 0.0 & 2.0 \end{bmatrix} u_t \\ \gamma_t &= \begin{bmatrix} 1.0 & -1.0 \end{bmatrix} x_t \\ 0 &\leq u_t \leq 1 \end{aligned}$$

A stationary point is given by

$$\begin{aligned} x^s &= \begin{bmatrix} 1.67 & 14.17 \\ -1.67 & 5.83 \end{bmatrix} u^s \\ \gamma^s &= \begin{bmatrix} 3.33 & 8.33 \end{bmatrix} u^s \end{aligned}$$

Any reference  $\gamma^{\text{ref}} < 0$  or  $\gamma^{\text{ref}} > 11.66$  will be infeasible since  $0 \leq u_t \leq 1$ .  $\triangle$

It is useful to note that the number of controlled variables usually is smaller than the number of states, hence, there may exist several  $x^s$  that satisfy  $\gamma^{\text{ref}} = \gamma^s$ . If the dimension of the control input  $u_t$  is larger than the dimension of the output  $\gamma_t$ , there may likewise exist several stationary controls  $u^s$  that satisfy  $\gamma^{\text{ref}} = \gamma^s$ . In this case we may specify preferred values for some of the control inputs.

$$\begin{aligned} f(z) &= \sum_{t=0}^{N-1} \frac{1}{2} (\gamma_{t+1} - \gamma_{t+1}^{\text{ref}})^\top Q (\gamma_{t+1} - \gamma_{t+1}^{\text{ref}}) \\ &\quad + \frac{1}{2} (u_t - u^{\text{ref}})^\top R (u_t - u^{\text{ref}}) + \frac{1}{2} \Delta u_t^\top R_\Delta \Delta u_t \quad (4.12) \end{aligned}$$

$u^{\text{ref}}$  defines reference control input values and  $R \succeq 0$ . It may be noted that this objective is covered by (4.1a). We will subsequently explore the extra degrees of freedom by returning to the example above.

**Example 10** (Feasibility of a stationary point — revisited)

Assume a feasible reference output  $\gamma^{\text{ref}} = 2.0$  in the previous example. This may be realized by an (infinite) number of control input combinations. Three of these options are  $u^s = \begin{bmatrix} 0.00 \\ 0.24 \end{bmatrix}$  or  $u^s = \begin{bmatrix} 0.17 \\ 0.17 \end{bmatrix}$  or  $u^s = \begin{bmatrix} 0.60 \\ 0.00 \end{bmatrix}$ . In this case the second choice will usually be preferred since both control inputs then operate away from their limits, i.e., none of the control input constraints are active. Hence, in the case of a dynamic disturbance both control inputs can move in both directions to compensate for the disturbance.  $\triangle$



The selection of reference outputs is not treated herein, apart from a discussion in the later Section 4.6.1 where it is treated in the context of the control hierarchy.

Integral action is an important feature of PID controllers and provides the means to compensate for disturbances with a bias component. In other words we want some controlled variables, which are measured, to converge to a constant reference value despite a constant disturbance<sup>10</sup>.

We will now discuss how integral action can be embedded in an MPC controller and show one way of doing this. We impose integral action on the controlled variables  $\gamma_t$ , meaning that we want  $\gamma_t$  to approach a constant reference  $\gamma^{\text{ref}}$  in spite of a constant disturbance. The online measurements are as earlier defined by the output vector  $y_t$ , and we make the common assumption that integral action is imposed on all or some of the variables that are measured. Viewing the output model and the model for the controlled variables, respectively,

$$y_t = Cx_t \quad (4.13a)$$

$$\gamma_t = Hx_t \quad (4.13b)$$

Since we impose integral action on all or some of the measured variables  $y_t$ , then  $H$  will contain a subset of the rows of  $C$ .

The basis for the approach taken here is to extend the dynamic model with a disturbance model,

$$\begin{aligned} \begin{bmatrix} x_{t+1} \\ d_{t+1} \end{bmatrix} &= \begin{bmatrix} A & A_d \\ 0 & I \end{bmatrix} \begin{bmatrix} x_t \\ d_t \end{bmatrix} + \begin{bmatrix} B \\ 0 \end{bmatrix} u_t \\ y_t &= \begin{bmatrix} C & C_d \end{bmatrix} \begin{bmatrix} x_t \\ d_t \end{bmatrix} \end{aligned}$$

and the idea is to accurately estimate the disturbance. We observe that the disturbance model is an integrating model. The augmented model, including the states and disturbances, are estimated using a state estimator as discussed in Section 4.2.3. Taking a stochastic viewpoint, as briefly commented upon in that section, noise is added to the dynamic model and the output model, and thus the state estimator updates an augmented state vector  $(x_t, d_t)^\top$  as shown below.

$$\begin{bmatrix} \hat{x}_{t+1} \\ \hat{d}_{t+1} \end{bmatrix} = \begin{bmatrix} A & A_d \\ 0 & I \end{bmatrix} \begin{bmatrix} \hat{x}_t \\ \hat{d}_t \end{bmatrix} + \begin{bmatrix} B \\ 0 \end{bmatrix} u_t + \begin{bmatrix} K_F \\ K_d \end{bmatrix} (y_t - \hat{y}_t) \quad (4.14a)$$

$$\hat{y}_t = \begin{bmatrix} C & C_d \end{bmatrix} \begin{bmatrix} \hat{x}_t \\ \hat{d}_t \end{bmatrix} \quad (4.14b)$$

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<sup>10</sup>One may seek zero offset for a time varying reference signal. This is, however, beyond the scope of this exposition.

An estimate of the controlled variable is then given by

$$\hat{\gamma}_t = H\hat{x}_t \quad (4.15)$$

and integral action is obtained by replacing the measured control variable  $\gamma_t$  with its estimate  $\hat{\gamma}_t$  given by (4.14) and (4.15) in an appropriate objective function. A typical objective is given below.

$$f(z) = \sum_{t=0}^{N-1} \frac{1}{2} (\hat{\gamma}_t - \gamma^{\text{ref}})^\top Q (\hat{\gamma}_t - \gamma^{\text{ref}}) + \frac{1}{2} \Delta u_t^\top R_\Delta u_t \quad (4.16)$$

It may be useful to compare (4.16) with (4.11). There are two differences. First, we use a constant reference in (4.16) instead of a time varying reference since we focus on the constant reference case. Second, the measured output  $y_t$  is corrupted by the disturbance  $d_t$ , and thus this also holds for the controlled variables  $\gamma_t$ . Therefore we use the estimate  $\hat{\gamma}_t$  in the objective function.

We use a simple example to explain the importance of the noise model in the state estimator.

**Example 11** (Integral action and noise model)

Assume a first order model, which is open loop stable.

$$\begin{aligned} x_{t+1} &= ax_t + bu_t \\ y_t &= x_t + n_t \\ |a| &< 1 \\ \gamma_t &= x_t \end{aligned}$$

$n_t$  is the measurement noise and the controlled variable equals the state. We assume constant noise  $n_t = \bar{n}$  and constant control  $u_t = \bar{u}$ . The stationary solution is given by

$$\begin{aligned} \bar{x} &= \frac{b}{1-a} \bar{u} \\ \bar{y} &= \bar{x} + \bar{n} = \frac{b}{1-a} \bar{u} + \bar{n} \\ \bar{\gamma} &= \bar{x} = \frac{b}{1-a} \bar{u} \end{aligned}$$

We will now test two different estimators starting with the simplest option.

$$\begin{aligned} \hat{x}_{t+1} &= a\hat{x}_t + bu_t + k(y_t - \hat{y}_t) \\ \hat{y}_t &= \hat{x}_t \end{aligned}$$

The stationary value of the state estimate is given by

$$\begin{aligned}\hat{x} &= a\hat{x} + b\bar{u} + k(\bar{y} - \hat{y}) \\ \hat{y} &= \hat{x} \\ \Downarrow \\ \hat{x} &= \frac{b}{1-a}\bar{u} + \frac{k}{1-a+k}\bar{n} \\ \hat{\gamma} &= \frac{b}{1-a}\bar{u} + \frac{k}{1-a+k}\bar{n}\end{aligned}$$

and we immediately observe that  $\hat{\gamma}$  differ  $\bar{\gamma}$  from when  $\bar{n} \neq 0$ . Thus, there will be a bias in the state estimate in this case and therefore a bias in the controlled variables, i.e.,  $\bar{\gamma} \neq \gamma^{\text{ref}}$ .

The estimator will subsequently be extended with a noise model

$$\begin{aligned}\hat{x}_{t+1} &= a\hat{x}_t + bu_t + k(y_t - \hat{y}_t) \\ \hat{d}_{t+1} &= \hat{d}_t + k_d(y_t - \hat{y}_t) \\ \hat{y}_t &= \hat{x}_t + \hat{d}_t\end{aligned}$$

where  $\hat{d}_t$  is an estimate of the measurement noise. In this case the stationary value of the state estimate is given by

$$\begin{aligned}\hat{x} &= a\hat{x} + b\bar{u} + k(\bar{y} - \hat{y}) \\ \hat{d} &= \hat{d} + k_d(\bar{y} - \hat{y}) \\ \hat{y} &= \hat{x} + \hat{d} \\ \Downarrow \\ \hat{x} &= \frac{b}{1-a}\bar{u} + \frac{k}{1-a+k}(\bar{n} - \hat{d}) \\ \hat{d} &= \hat{d} + k_d(\bar{y} - \hat{y}) \\ \Downarrow \\ \hat{x} &= \frac{b}{1-a}\bar{u} + \frac{k}{1-a+k}(\bar{n} - \hat{d}) \\ \hat{d} &= \hat{d} + \frac{k_d b}{1-a}\bar{u} + k_d \bar{n} - k_d \hat{x} - k_d \hat{d} \\ \Downarrow \\ \hat{x} &= \frac{b}{1-a}\bar{u} + \frac{k}{1-a+k}(\bar{n} - \hat{d}) \\ \hat{d} &= \bar{n} \\ \Downarrow\end{aligned}$$

$$\hat{\gamma} = \hat{x} = \frac{b}{1-a}\bar{u}$$

Hence, the constant disturbance does not affect the estimate of the controlled variable and it is thus an accurate estimate. If we apply objective function (4.16) and replace  $\gamma_t$  with its estimate, the (stationary) solution is  $\hat{\gamma}_t = \gamma^{\text{ref}}$  and  $\Delta u_t = 0$  provided (possible) inequality constraints allow for this solution. Since there is no bias in the stationary estimate, integral action is guaranteed, that is,  $\bar{\gamma} = \gamma^{\text{ref}}$ .  $\triangle$

Integral action on  $\gamma_t$  will not always be feasible. First, the dimension of  $\gamma_t$ , i.e., the number of variables with integral action, cannot exceed the number of control inputs. Second, if some of the control inputs saturate, some degrees of freedom are lost. One may thus lose integral action on some of the control variables. Useful material on tracking and integral action can be found in Rawlings and Mayne (2009).

## 4.3 Linear Quadratic control

In this section we remove the inequality constraints altogether. First, the finite horizon LQ problem is presented and analyzed. Thereafter it is compared to the linear MPC case. Second, the infinite horizon LQ problem is discussed. This problem is subsequently discussed in the context of output feedback.

### 4.3.1 Finite horizon LQ control

We now remove all inequalities from (4.1) and pose the following problem.

$$\min_{z \in \mathbb{R}^n} f(z) = \sum_{t=0}^{N-1} \frac{1}{2} x_{t+1}^\top Q_{t+1} x_{t+1} + \frac{1}{2} u_t^\top R_t u_t \quad (4.17a)$$

subject to

$$x_{t+1} = A_t x_t + B_t u_t \quad (4.17b)$$

$$x_0 = \text{given} \quad (4.17c)$$

where

$$z^\top = (x_1^\top, \dots, x_N^\top, u_0^\top, \dots, u_{N-1}^\top) \quad (4.17d)$$

$$n = N \cdot (n_x + n_u) \quad (4.17e)$$

The linear terms and the quadratic  $\Delta u_t$  term have also been removed from the objective function in addition to the inequality constraints. This will be commented later. (4.17) is usually called the LQ problem. Referring to Chapter 16.1 in Nocedal and Wright (2006) we should expect an explicit solution in this case as opposed to linear MPC which includes inequality constraints. We will now show that the solution of the LQ problem can be written in closed form. Moreover, this closed form is given as a linear state feedback controller, i.e.,  $u_t = K_t x_t$ .

**Theorem 3** (LQ control and the Riccati equation).

*The solution of (4.17) with  $Q_t \succeq 0$  and  $R_t \succ 0$  is given by*

$$u_t = -K_t x_t \quad (4.18a)$$

where the feedback gain matrix is derived by

$$K_t = R_t^{-1} B_t^\top P_{t+1} (I + B_t R_t^{-1} B_t^\top P_{t+1})^{-1} A_t, \quad t = 0, \dots, N-1 \quad (4.18b)$$

$$P_t = Q_t + A_t^\top P_{t+1} (I + B_t R_t^{-1} B_t^\top P_{t+1})^{-1} A_t, \quad t = 0, \dots, N-1 \quad (4.18c)$$

$$P_N = Q_N \quad (4.18d)$$

*Proof. Part 1: KKT conditions*

Define the Lagrange function

$$\begin{aligned} \mathcal{L}(z, \lambda_1, \dots, \lambda_N) &= \sum_{t=0}^{N-1} \frac{1}{2} x_{t+1}^\top Q_{t+1} x_{t+1} + \frac{1}{2} u_t^\top R_t u_t \\ &\quad - \sum_{t=0}^{N-1} \lambda_{t+1}^\top (x_{t+1} - A_t x_t - B_t u_t) \end{aligned}$$

The KKT conditions, see e.g., Chapter 12 in Nocedal and Wright (2006), are given by<sup>11</sup>

$$\frac{\partial}{\partial u_t} \mathcal{L}(z, \lambda_1, \dots, \lambda_N) = R_t u_t + B_t^\top \lambda_{t+1} = 0, \quad t = 0, \dots, N-1 \quad (4.19a)$$

$$\frac{\partial}{\partial x_t} \mathcal{L}(z, \lambda_1, \dots, \lambda_N) = Q_t x_t - \lambda_t + A_t^\top \lambda_{t+1} = 0, \quad t = 1, \dots, N-1 \quad (4.19b)$$

$$\frac{\partial}{\partial x_N} \mathcal{L}(z, \lambda_1, \dots, \lambda_N) = Q_N x_N - \lambda_N = 0 \quad (4.19c)$$

and (4.17b) and (4.17c).<sup>12</sup>

<sup>11</sup>We skip the definition of the index set, e.g.,  $t = 0, \dots, N-1$ , many places below to simplify notation.

<sup>12</sup>Equation (4.19b) can be difficult to apprehend. Hence, it may be useful to derive it from scratch for a simple example.

Since  $R_t$  is positive definite, it is also invertible. Then, (4.19a) gives

$$u_t = -R_t^{-1}B_t^\top \lambda_{t+1} \quad (4.20)$$

We use (4.19c) to postulate that the Lagrange multipliers  $\lambda_t$  depend linearly on the states  $x_t$ .

$$\lambda_t = P_t x_t \quad (4.21)$$

This gives

$$P_N = Q_N \quad (4.22)$$

We substitute (4.20) and (4.21) into (4.17b)

$$x_{t+1} = A_t x_t + B_t(-R_t^{-1}B_t^\top P_{t+1}x_{t+1})$$

and, solving for  $x_{t+1}$ , we obtain

$$x_{t+1} = (I + B_t R_t^{-1} B_t^\top P_{t+1})^{-1} A_t x_t \quad (4.23)$$

Then, we substitute (4.21) into (4.19b)

$$Q_t x_t - \lambda_t + A_t^\top \lambda_{t+1} = Q_t x_t - P_t x_t + A_t^\top P_{t+1} x_{t+1} = 0 \quad (4.24)$$

Now  $x_{t+1}$  can be removed from (4.24) by using (4.23)

$$Q_t x_t - P_t x_t + A_t^\top P_{t+1} (I + B_t R_t^{-1} B_t^\top P_{t+1})^{-1} A_t x_t = 0$$

Since  $x_t$  is a common factor, we can write

$$(Q_t - P_t + A_t^\top P_{t+1} (I + B_t R_t^{-1} B_t^\top P_{t+1})^{-1} A_t) x_t = 0$$

This equality must hold for any  $x_t$ , in particular it must hold for  $x_t \neq 0$ . This gives

$$Q_t - P_t + A_t^\top P_{t+1} (I + B_t R_t^{-1} B_t^\top P_{t+1})^{-1} A_t = 0,$$

which we recognize as (4.18c).

Now, (4.20), (4.21) and (4.23) give

$$\begin{aligned} u_t &= -R_t^{-1} B_t^\top P_{t+1} x_{t+1} \\ &= -R_t^{-1} B_t^\top P_{t+1} (I + B_t R_t^{-1} B_t^\top P_{t+1})^{-1} A_t x_t \\ &= -K_t x_t \end{aligned}$$

This shows that (4.18) satisfies the KKT conditions.

*Part 2: Second order conditions*

Note that the states  $x_1, \dots, x_N$  can be written:

$$\begin{aligned} \chi &= \begin{bmatrix} x_1 \\ x_2 \\ \vdots \\ x_{N-1} \\ x_N \end{bmatrix} = \begin{bmatrix} A_0 \\ A_1 A_0 \\ \vdots \\ A_{N-2} \cdots A_0 \\ A_{N-1} \cdots A_0 \end{bmatrix} x_0 \\ &+ \begin{bmatrix} B_0 & 0 & \cdots & 0 & 0 \\ A_1 B_0 & B_1 & \ddots & \vdots & \vdots \\ \vdots & \vdots & \ddots & 0 & 0 \\ A_{N-2} \cdots A_1 B_0 & A_{N-2} \cdots A_2 B_1 & \cdots & B_{N-2} & 0 \\ A_{N-1} \cdots A_1 B_0 & A_{N-1} \cdots A_2 B_1 & \cdots & A_{N-1} B_{N-2} & B_{N-1} \end{bmatrix} v \\ &= \widehat{A}x_0 + \widehat{B}v \end{aligned} \quad (4.25)$$

where

$$v^\top = (u_0^\top, \dots, u_{N-1}^\top)$$

We define the following matrices

$$\widehat{Q}_0 = \begin{bmatrix} Q_1 & 0 & \cdots & 0 & 0 \\ 0 & Q_2 & \ddots & \vdots & \vdots \\ 0 & 0 & \ddots & 0 & 0 \\ \vdots & \vdots & \ddots & Q_{N-1} & 0 \\ 0 & 0 & \cdots & 0 & Q_N \end{bmatrix} \quad (4.26a)$$

$$\widehat{R}_0 = \begin{bmatrix} R_0 & 0 & \cdots & 0 & 0 \\ 0 & R_1 & \ddots & \vdots & \vdots \\ 0 & 0 & \ddots & 0 & 0 \\ \vdots & \vdots & \ddots & R_{N-2} & 0 \\ 0 & 0 & \cdots & 0 & R_{N-1} \end{bmatrix} \quad (4.26b)$$

By using (4.25) and (4.26) the objective function (4.17a) may be written as a function of  $v$  instead of  $z$ , meaning that the states  $x_1, \dots, x_N$  are eliminated through the equality constraints.

$$\begin{aligned}
f(z) = g(v) &= \frac{1}{2}\chi^\top \widehat{Q}_0 \chi + \frac{1}{2}v^\top \widehat{R}_0 v + \frac{1}{2}x_0^\top Q_0 x_0 \\
&= \frac{1}{2}(\widehat{A}x_0 + \widehat{B}v)^\top \widehat{Q}_0 (\widehat{A}x_0 + \widehat{B}v) + \frac{1}{2}v^\top \widehat{R}_0 v + \frac{1}{2}x_0^\top Q_0 x_0 \\
&= \frac{1}{2}v^\top (\widehat{R}_0 + \widehat{B}^\top \widehat{Q}_0 \widehat{B})v + x_0^\top \widehat{A}^\top \widehat{Q}_0 \widehat{B}v + \frac{1}{2}x_0^\top (Q_0 + \widehat{A}^\top \widehat{Q}_0 \widehat{A})x_0.
\end{aligned}$$

Thus, minimizing  $g(v)$  without equality constraints is equal to the original LQ problem. Note that  $\widehat{R}_0 + \widehat{B}^\top \widehat{Q}_0 \widehat{B}$  is positive definite since  $\widehat{R}_0$  is positive definite<sup>13</sup> and  $\widehat{B}^\top \widehat{Q}_0 \widehat{B}$  is positive semidefinite<sup>14</sup>. Hence,  $g(v)$  is a strictly convex function and second order conditions are therefore satisfied.<sup>15</sup>

*Part 3: Summing up*

We choose to use Theorem 12.6 in Nocedal and Wright (2006) to show sufficiency.

- a) (4.18) satisfies the KKT conditions.
- b) In Part 2 of the proof we showed that  $g(v)$  is a strictly convex function and (12.65) in Nocedal and Wright (2006) will hence be satisfied.
- c) The LQ problem is a strictly convex problem; hence the solution is a unique global solution.<sup>16</sup>

□

There are several interesting features related to the LQ solution. We note that the solution can be formulated as a state feedback controller as shown in Figure 4.4. The controller is a linear time varying (LTV) controller. It is important to note that *the gain matrix  $K_k$  can be computed independently of the states*. It only depends on the system matrices  $(A_t, B_t)$  and the weighting matrices in the objective function  $(Q_t, R_t)$ . It can hence be computed and stored prior to the actual use of the solution.

(4.18c) is the well known *discrete Riccati equation*. It is a discrete time nonlinear matrix equation. A special feature of this equation is the fact that the boundary condition is given at the end of the optimization horizon as shown in (4.18d). This implies that the sequence of matrices  $(P_1, P_2, \dots, P_{N-1})$

<sup>13</sup>Remember that  $R_t$  is assumed to be positive definite.

<sup>14</sup>The reason is that  $\widehat{Q}_0$  is positive semidefinite and hence  $\widehat{B}^\top \widehat{Q}_0 \widehat{B}$  will be positive semidefinite

<sup>15</sup>Theorem 12.6 in Nocedal and Wright (2006) will for instance be satisfied.

<sup>16</sup>As opposed to a local solution as in Theorem 12.6 in Nocedal and Wright (2006).



is computed by iterating (4.18c) backwards in time. Note that these matrices are necessary to obtain the gain matrices  $(K_0, K_1, \dots, K_{N-1})$  as shown in (4.18b).

The matrices  $(P_1, P_2, \dots, P_N)$  are known as the Riccati matrices. They are symmetric positive semidefinite matrices. To ensure that this property is retained during computation (4.18d) it is usually substituted by some equivalent equation with improved numerical properties. One example is

$$P_t = Q_t + A_t^\top (P_{t+1}^{-1} + B_t R_t^{-1} B_t^\top)^{-1} A_t.$$

In the event of an LTI system and constant weight matrices (4.18) is slightly simplified.

$$K_t = R^{-1} B^\top P_{t+1} (I + B R^{-1} B^\top P_{t+1})^{-1} A, \quad t = 0, \dots, N-1 \quad (4.27a)$$

$$P_t = Q + A^\top P_{t+1} (I + B R^{-1} B^\top P_{t+1})^{-1} A, \quad t = 0, \dots, N-1 \quad (4.27b)$$

$$P_N = Q \quad (4.27c)$$

It is important to note that the feedback gain  $(K_t)$  is time varying even though the system and weighting matrices are time invariant.

The tuning parameters of the LQ controller are the weighting matrices  $(Q_t, R_t)$ . To make an analogy, in a SISO PI controller we adjust the gain and integral time as opposed to the weighting matrices in a LQ controller. As a side remark we note that the LQ controller is a MIMO controller since the dimensions of the control input and states usually are greater than one.

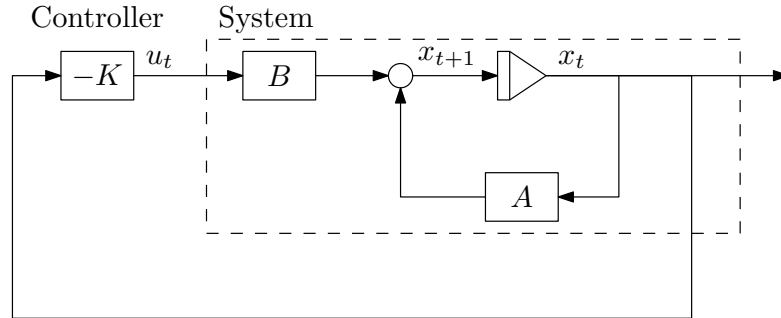


Figure 4.4: Solution of the LQ control problem, i.e., with state feedback.

A deeper understanding of how to select weighting matrices can only be achieved through experience. Some insight can be obtained by inspection of the equations. In particular increased values of the (diagonal) elements of  $R_t$  reduces the gain of the LQ controller. This becomes quite clear by noting that  $K_t = R_t^{-1} B_t^\top P_{t+1} (I + B_t R_t^{-1} B_t^\top P_{t+1})^{-1} A_t \approx R_t^{-1} B_t^\top P_{t+1} A_t$  when  $R_t$  is large. To provide some additional insight we present a simple example similar to an example used earlier.

**Example 12** (LQ control and tuning)

Assume a simple first order system

$$x_{t+1} = 1.2x_t + u_t \quad (4.28a)$$

$$x_0 = 1 \quad (4.28b)$$

and an objective function where  $N = 11$ .

$$f(z) = \sum_{t=0}^{10} \frac{1}{2} x_{t+1}^2 + \frac{1}{2} r u_t^2, \quad r > 0 \quad (4.28c)$$

The Riccati equation is given by

$$\begin{aligned} P_t &= 1 + 1.2P_{t+1}(1 + r^{-1} \cdot P_{t+1})^{-1}1.2 \\ &= 1 + \frac{1.44r P_{t+1}}{P_{t+1} + r}, \quad t = 0, \dots, 10 \end{aligned} \quad (4.29a)$$

$$P_{11} = 1 \quad (4.29b)$$

and the gains are computed by

$$K_t = r^{-1}P_{t+1}(1 + r^{-1}P_{t+1})^{-1}1.2 = 1.2 \frac{P_{t+1}}{P_{t+1} + r}, \quad t = 0, \dots, 10 \quad (4.29c)$$

The controller may be written as

$$u_t = -K_t x_t, \quad t = 0, \dots, 10 \quad (4.29d)$$

Figure 4.5 shows the Riccati matrix, which is a scalar in this example, and the controller gain. The controller gain is clearly time varying even though the system and weight matrices are time invariant. Further, the controller gain increases with a reduced value of  $r$ . Figure 4.6 shows the state  $x_t$  and the control input  $u_t$ . It is quite apparent from this figure that the bandwidth of the controller increases with a decrease in  $r$ .  $\triangle$

As in Section 3.3 we may include a reference trajectory by including a term like  $(x_{t+1} - x_{t+1}^{\text{ref}})^\top Q_{t+1} (x_{t+1} - x_{t+1}^{\text{ref}})$  in the objective function. This will however extend the optimal solution with a feedforward term from the reference<sup>17</sup>.

<sup>17</sup>The solution will in this case actually require knowledge of the future reference trajectory at a given time  $t$ , see e.g., Anderson and Moore (1990).

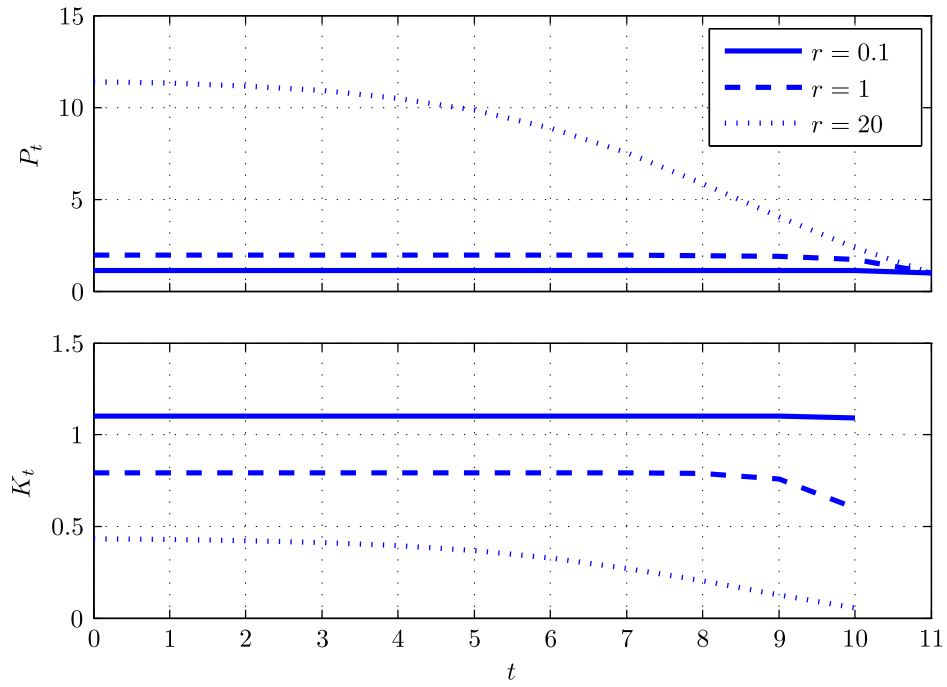


Figure 4.5: The figure shows  $P_t$  and the controller gain  $K_t$ . Solid line:  $r = 0.1$ . Dashed line:  $r = 1$ . Dotted line:  $r = 20$ .

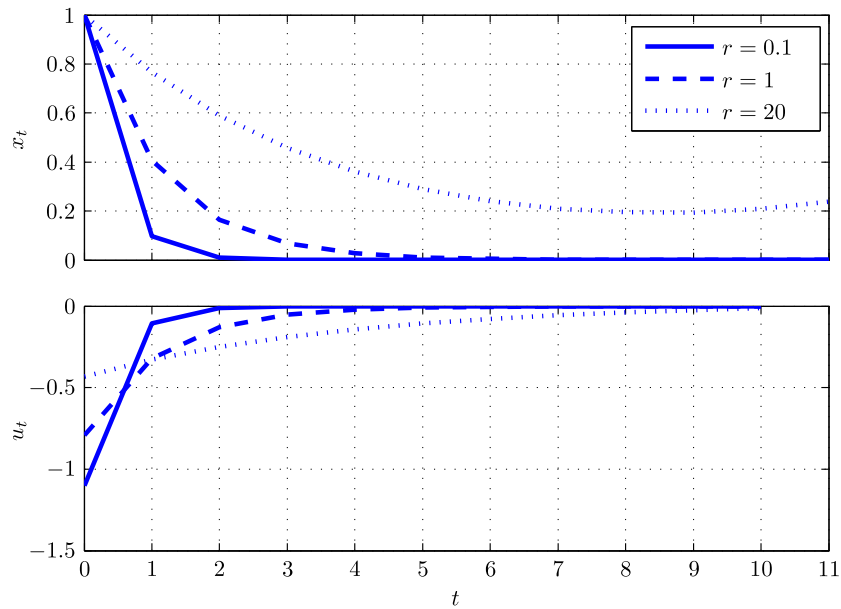


Figure 4.6: The figure shows the state  $x_t$  and the control input  $u_t$ . Solid line:  $r = 0.1$ . Dashed line:  $r = 1$ . Dotted line:  $r = 20$ .

### 4.3.2 Moving horizon LQ control

Linear MPC, and finite horizon LQ control as discussed above, do have significant similarities. By removing the inequality constraints from linear MPC we find a simple closed form solution for the LQ problem. Hence, the computation at each time step is reduced to a simple matrix multiplication instead of solving a QP problem. This is observed by comparing (4.18a) with Algorithm 2, i.e. state feedback MPC.

The LQ controller is the solution of an open loop optimization problem even though the solution appears as a state feedback controller. The structure of the solution, however, accommodates a closed loop solution in a straightforward way. We just repeat the solution on a moving horizon. In this case  $K_t$  will be constant for all  $t$  for an LTI system with constant weight matrices, cf. (4.27), as opposed to the open loop solution in which  $K_t$  varies from one time step to the next.

In the output feedback case (4.18a) is replaced by

$$u_t = -K_t \hat{x}_t \quad (4.30)$$

where  $\hat{x}_t$  is the state estimate. The algorithm is shown in Algorithm 6.

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#### Algorithm 6 Output feedback moving horizon LQ

---

**for**  $t = 0, 1, 2, \dots$  **do**

    Compute an estimate of the current state  $\hat{x}_t$  based on the data up until time  $t$ .

    Compute and apply the control  $u_t = -K_t \hat{x}_t$ .  $K_t$  will be constant for all  $t$  for an LTI system and an objective function with constant weight matrices.

**end for**

---

## 4.4 Infinite horizon LQ control

In the above section the optimal controller was an LTV controller. We will now develop an even simpler controller by seeking a controller with a constant feedback gain, that is  $u_t = -Kx_t$ . We start with the state feedback case.

### 4.4.1 State feedback infinite horizon LQ control

To guide the search we observe from Figure 4.5 that the gain seems to settle to some stationary value after some iterations.<sup>18</sup> This is a general property of the Riccati equation provided the system satisfies certain conditions to be defined later. By increasing the horizon sufficiently it should therefore be possible to obtain an optimal controller with a constant gain matrix within any time interval of interest provided  $A$ ,  $B$ ,  $Q$  and  $R$  do not vary with time. This is the basis for the infinite horizon LQ controller where we optimize on an infinite time horizon, i.e.,  $N \rightarrow \infty$ . The problem is formulated as follows:

$$\min_z f^\infty(z) = \sum_{t=0}^{\infty} \frac{1}{2} x_{t+1}^\top Q x_{t+1} + \frac{1}{2} u_t^\top R u_t \quad (4.31a)$$

subject to equality constraints

$$x_{t+1} = Ax_t + Bu_t \quad (4.31b)$$

$$x_0 = \text{given} \quad (4.31c)$$

and

$$Q \succeq 0 \quad (4.31d)$$

$$R \succ 0 \quad (4.31e)$$

where system dimensions are given by

$$u_t \in \mathbb{R}^{n_u} \quad (4.31f)$$

$$x_t \in \mathbb{R}^{n_x} \quad (4.31g)$$

$$z^\top = (u_0^\top, \dots, u_\infty^\top, x_1^\top, \dots, x_\infty^\top) \quad (4.31h)$$

There are some issues that need clarification before presenting the solution.

- Problem (4.31) is an infinite dimensional QP problem since  $n \rightarrow \infty$  in (4.31a). Hence, it cannot be solved using a conventional method since the *KKT matrix* is infinitely large and hence not well defined<sup>19</sup>.
- The objective function must be bounded above, i.e.,  $f^\infty(z) < \infty$ , for some feasible  $z$ . Inspection of the objective function shows that this implies that  $u_t \rightarrow 0$  when  $t \rightarrow \infty$ . Otherwise  $f^\infty(z) \rightarrow \infty$ .

<sup>18</sup>Remember that the Riccati matrix and thereby the gain is computed backwards in time.

<sup>19</sup>See e.g. Chapter 16 in Nocedal and Wright (2006) for a definition of the KKT matrix.

If the system (4.31b) is *stabilizable*<sup>20</sup> there will always exist a well defined solution of (4.31). Stabilizability is a weaker form of *controllability*<sup>21</sup>. It means that at least all the unstable modes of a system must be controllable. The relationship between controllability and stabilizability is therefore as follows:

System  $(A,B)$  is controllable  $\Rightarrow$  System  $(A,B)$  is stabilizable

We may now state a formal result on the existence of a solution to (4.31a)–(4.31b).

**Theorem 4.**

*Let (4.31b) be stabilizable. Then there exists a static solution to (4.27b), i.e.,  $P_t \rightarrow \bar{P}$  when  $t \rightarrow -\infty$ . This solution is equal to the unique positive semidefinite solution of the algebraic Riccati equation (4.32c).*

*Proof.* See Chapter 2 in Lewis (1986). □

Provided the above theorem is satisfied the infinite LQ controller is given as follows:

**Theorem 5.**

*The solution of (4.31) is given by*

$$u_t = -Kx_t \quad \text{for } 0 \leq t \leq \infty \quad (4.32a)$$

*where the feedback gain matrix is derived by*

$$K = R^{-1}B^T P(I + BR^{-1}B^T P)^{-1}A \quad (4.32b)$$

$$P = Q + A^T P(I + BR^{-1}B^T P)^{-1}A \quad (4.32c)$$

$$P = P^T \succeq 0 \quad (4.32d)$$

*Proof.* See Chapter 2 in Lewis (1986). □

The infinite horizon LQ controller  $u_t = -Kx_t$  is often called the *Linear Quadratic Regulator* or just *LQR*.

It should be noted that the algebraic Riccati-equation (4.32c) is a quadratic equation in the unknown matrix  $P$ . Thus, there may exist several solutions to this equation. Only one solution, however, will be positive semidefinite and therefore satisfy (4.32d).

<sup>20</sup>System  $(A,B)$  is stabilizable if all the uncontrollable modes are asymptotically stable.

<sup>21</sup>System  $(A,B)$  is controllable if for any initial state  $x_0$  and any final state  $x_N$ , there exists a finite number of inputs  $u_0, \dots, u_{N-1}$  to transfer  $x_0$  to  $x_N$ .

Returning to Example 12 the Riccati equation was equal to

$$P_t = 1 + \frac{1.44r P_{t+1}}{P_{t+1} + r}$$

The algebraic version, i.e., (4.32c) is obtained by choosing  $P_t = P_{t+1} = P$ .

$$P^2 + (r - 1 - 1.2^2r)P - r = 0$$

This equation has two solutions; one is positive and the other is negative. Hence, the positive solution is chosen.

A key difference between the finite and infinite LQ problem is the fact that the infinite LQ problem is defined on an infinite time horizon. Hence, stability becomes an important issue. We therefore formulate the following question: *Under which conditions will the closed loop system*

$$x_{t+1} = Ax_t + Bu_t = Ax_t - BKx_t = (A - BK)x_t \quad (4.33)$$

*be stable?* By stability we mean asymptotic stability, which implies that the states  $x_t \rightarrow 0$ , and thereby  $u_t \rightarrow 0$ , when  $t \rightarrow \infty$ .<sup>22</sup> The answer is given by the following theorem.

**Theorem 6.**

*Given problem (4.31). Let system  $(A, B)$ <sup>23</sup> be stabilizable and  $(A, D)$ <sup>24</sup> detectable.  $D$  is defined by  $Q = D^\top D$ . Then the closed loop system given by the optimal solution is asymptotically stable.*

*Proof.* See Chapter 2 in Lewis (1986). □

This theorem deserves some comments.

- *Detectability*<sup>25</sup> is a milder form of *observability*<sup>26</sup>. This implies that an observable system always is detectable. The opposite is however not necessarily true.

<sup>22</sup>The system  $x_{t+1} = Ax_t$  is asymptotically stable if the absolute value of the eigenvalues of  $A$  are less than 1, i.e.,  $|\lambda_i(A)| < 1$  for all  $1 \leq i \leq n_x$ , where  $\lambda_i(A)$  is the  $i$ th eigenvalue of  $A$ .

<sup>23</sup> $x_{t+1} = Ax_t + Bu_t$

<sup>24</sup>The system  $x_{t+1} = Ax_t$  or  $x_{t+1} = Ax_t + Bu_t$  is observed through the output  $y_t = Dx_t$

<sup>25</sup>System  $(A, D)$  is detectable if all the unobservable modes are asymptotically stable.

<sup>26</sup>System  $(A, D)$  is observable if the state  $x_N$  can be determined from the system model, its inputs and outputs for a finite number of steps.

- Since  $Q$  is positive semidefinite it will always be possible to find a  $D$  defined by  $Q = D^\top D$ . As an example if  $Q = \begin{bmatrix} 0 & 0 \\ 0 & 1 \end{bmatrix} \succeq 0$  we choose  $D = \begin{bmatrix} 0 & 1 \end{bmatrix}$ .<sup>27</sup>

The two conditions in Theorem 6 do have an intuitive interpretation. The stabilizability condition tells us that we must be able to influence all unstable modes. A system with unstable modes that cannot be influenced by the control input will namely remain unstable for all control designs. The objective function must be sensitive to all the unstable modes to satisfy the detectability condition. In the opposite case a state may go to infinity without influencing the value of the objective function. Hence, unboundedness of such a state cannot be guaranteed in this situation.

**Example 13** (Stability on an infinite horizon LQ controller)

To elaborate on Theorem 6 we study the following system

$$x_{t+1} = \begin{bmatrix} 1.2 & 0 \\ 0 & 0.8 \end{bmatrix} x_t + \begin{bmatrix} b_1 \\ b_2 \end{bmatrix} u_t, \quad x_0 = \begin{bmatrix} 1 \\ 1 \end{bmatrix} \quad (4.34)$$

with the weight matrices

$$Q = I = \begin{bmatrix} 1 & 0 \\ 0 & 1 \end{bmatrix}, \quad R = 1 \quad (4.35)$$

It may be noted that (4.34) is an open loop unstable system since one of the eigenvalues is outside the unit circle.

If  $b_1 \neq 0$  and  $b_2 \neq 0$  the system  $(A, B)$  is stabilizable. It is even controllable. Further,  $(A, D)$  is detectable, and also observable since  $Q = \begin{bmatrix} 1 & 0 \\ 0 & 1 \end{bmatrix}$

and thereby  $D = \begin{bmatrix} 1 & 0 \\ 0 & 1 \end{bmatrix}$ . Therefore the infinite LQ controller will stabilize the system, i.e., the eigenvalues of  $(A - BK)$  will lie inside the unit circle.

The system will not be stabilizable if  $b_1 = 0$  since the first state will grow independently of the control action, i.e.,  $x_{1,t} \rightarrow \pm\infty$  as  $t \rightarrow \infty$  provided  $x_0 \neq 0$ . As a side remark one may note that the system is stabilizable, but not controllable, if  $b_1 \neq 0$  and  $b_2 = 0$ .

The objective function will not be influenced by the first state  $x_{1,t}$  if  $Q$  is changed to  $Q = \begin{bmatrix} 0 & 0 \\ 0 & 1 \end{bmatrix}$  since system  $(A, D)$ , where  $D = \begin{bmatrix} 0 & 1 \end{bmatrix}$ , will

---

<sup>27</sup>Since  $\text{rank}(Q) = 1$  in this case,  $D$  will be a  $1 \times 2$  matrix. Hence, a  $2 \times 2$  matrix is no valid decomposition as opposed to (4.35) where  $\text{rank}(Q) = 2$ .



not be detectable. In the latter case  $D$  is a  $2 \times 2$  matrix. If  $Q = \begin{bmatrix} 1 & 0 \\ 0 & 0 \end{bmatrix}$  then  $D = \begin{bmatrix} 1 & 0 \end{bmatrix}$  and  $(A, D)$  is detectable. The system is, however, not observable in this case.

△

A further analysis of the closed loop system, provided Theorem 6 is satisfied, can be of interest. The infinite horizon LQ controller has excellent stability margins. Safonov and Athans (1977) showed that the controller has a 60 degree *phase margin* and 6 dB *gain margin*. This result depends on one critical assumption, however, a state feedback controller. As argued in the MPC section the states must be estimated and thus an output feedback algorithm, similar to Algorithm 3, will in practice be the only realistic option. In this case nominal stability can be proven, although without any stability margin. This was shown in an elegant paper by Doyle (1978). The combination of an LQ controller and a Kalman filter is usually denoted a *linear quadratic Gaussian (LQG)* controller since the Kalman filter initially was based on stochastic linear models with Gaussian white noise.

#### 4.4.2 Output feedback infinite horizon LQ control

To gain further insight on LQ control we analyze the output feedback case in an LTI setting. We combine the system (4.31b)–(4.31c) with a measurement model  $y_t = Cx_t$ , the output feedback LQ controller  $u_t = -K\hat{x}_t$ , and the Kalman filter (4.8).

$$x_{t+1} = Ax_t + Bu_t \quad (4.36a)$$

$$y_t = Cx_t \quad (4.36b)$$

$$u_t = -K\hat{x}_t \quad (4.36c)$$

$$x_0 = \text{given} \quad (4.36d)$$

$$\hat{x}_{t+1} = A\hat{x}_t + Bu_t + K_F(y_t - \hat{y}_t) \quad (4.36e)$$

$$\hat{y}_t = C\hat{x}_t \quad (4.36f)$$

$$\hat{x}_0 = \text{given} \quad (4.36g)$$

These equations can be rewritten in a compact form

$$\xi_{t+1} = \begin{bmatrix} x_{t+1} \\ \tilde{x}_{t+1} \end{bmatrix} = \begin{bmatrix} A - BK & BK \\ 0 & A - K_F C \end{bmatrix} \xi_t \quad (4.37)$$

$$\tilde{x}_t = x_t - \hat{x}_t$$

$$\xi_0 = \text{given}$$

where the dimension of the augmented state is given by

$$\xi_t \in \mathbb{R}^{2n_x}$$

and  $\tilde{x}_t$  refers to the error in the state estimates. The overall structure of the LQG controller is shown in Figure 4.7.

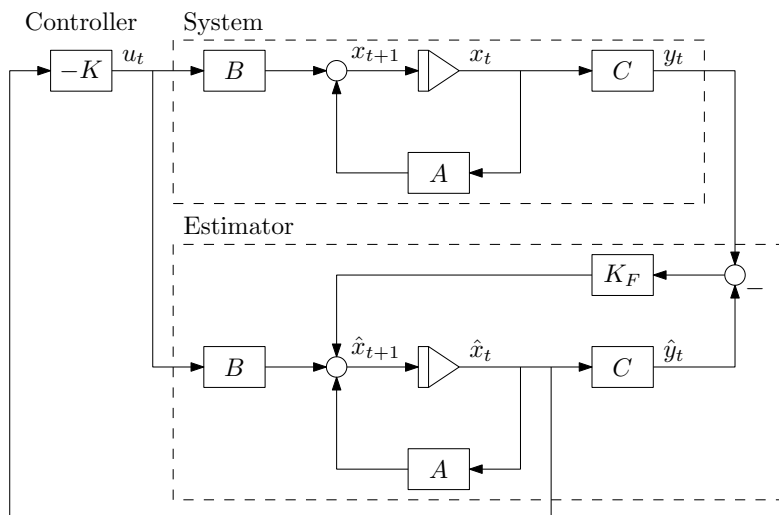


Figure 4.7: Structure of the LQG controller, i.e., output feedback LQ control.

Several comments and observations can be made from this.

- The dimension of the system and the state estimator is  $2 \cdot n_x$ , i.e., double the size of the original system. This reason is that the estimator introduces dynamics. To repeat, in the state feedback case the closed loop system has  $n_x$  eigenvalues while in the output feedback case the closed loop system has  $2 \cdot n_x$  eigenvalues.
- The dynamics of the matrix in (4.37) are given by the eigenvalues of  $A - BK$  and  $A - K_F C$ , respectively, since there is a 0 matrix in the lower left corner. Hence the eigenvalues are given by the dynamics of state feedback LQ control, i.e.,  $A - BK$ , and the estimator dynamics  $A - K_F C$ . This simplifies tuning since the estimator and controller can be tuned separately. As discussed earlier the estimator dynamics should be significantly faster than the LQ controller dynamics to limit interaction between these loops.
- (4.37) defines the system dynamics in an idealized case since the estimator model equals the system model. In practice there will always be

model errors. Model errors corrupt the matrix structure by for instance introducing non negative terms in the lower left matrix. Nevertheless, separation of dynamics according to (4.37) provide guidelines for tuning the estimator and controller provided the model is of a reasonable quality.

- The equation  $\xi_0 = \text{given}$  deserves a comment. The latter  $n_x$  elements of this vector defines the initial values for the errors in the state estimates.

### 4.4.3 Stability of linear MPC with infinite horizon LQ control

Based on the infinite horizon LQ stability result in Theorem 6 we continue the stability discussion of linear MPC in Section 4.2.2. We first simplify the linear MPC formulation (4.1) by removing the linear terms and the  $\Delta u_t$  term from the objective function, and select constant weight matrices and an LTI system. Further, we assume state feedback. Finally, (4.1) is changed by extending the prediction horizon to infinity.

$$\min_z f^\infty(z) = \sum_{t=0}^{\infty} \frac{1}{2} x_{t+1}^\top Q x_{t+1} + \frac{1}{2} u_t^\top R u_t \quad (4.38a)$$

subject to

$$x_{t+1} = A x_t + B u_t \quad (4.38b)$$

$$x_0 = \text{given} \quad (4.38c)$$

$$x^{\text{low}} \leq x_t \leq x^{\text{high}} \quad (4.38d)$$

$$u^{\text{low}} \leq u_t \leq u^{\text{high}} \quad (4.38e)$$

where

$$Q \succeq 0 \quad (4.38f)$$

$$R \succ 0 \quad (4.38g)$$

$$z^\top = (u_0^\top, \dots, u_\infty^\top, x_1^\top, \dots, x_\infty^\top) \quad (4.38h)$$

We first note that the origin is the only stationary point for the system. Otherwise the objective function will be unbounded.

This optimization problem may be split into two parts by dividing the prediction horizon into two parts:  $\{1, \dots, N-1\}$  and  $\{N, N+1, \dots\}$  (Muske and Rawlings, 1993; Chmielewski and Manousiouthakis, 1996; Scokaert and

Rawlings, 1998). The idea is to choose  $N$  such that the problem is unconstrained on the latter infinite horizon  $\{N, N + 1, \dots\}$ . Provided the system is controllable and  $N$  is large enough the system can be driven to a state  $x_N \in X'$ .  $X'$  is a set from where the latter optimal trajectory is unconstrained (Gilbert and Tan, 1991). This means that none of the state or control input constraints are active. The optimal objective function value on the latter horizon, usually referred to as the *value function*, is then given by

$$f_N^\infty(z^*) = \frac{1}{2}x_N^\top P x_N \quad (4.39a)$$

where

$$P = (A - BK)^\top P(A - BK) + K^\top R K + Q \quad (4.39b)$$

$K$  is the infinite horizon feedback gain, cf. (4.32b). The infinite horizon problem (4.38) may now be reformulated into a *finite dimensional QP problem*.

$$\min_z f^\infty(z) = \sum_{t=0}^{N-1} \frac{1}{2}x_{t+1}^\top Q x_{t+1} + \frac{1}{2}u_t^\top R u_t + f_N^\infty(z^*) \quad (4.40a)$$

subject to

$$x_{t+1} = Ax_t + Bu_t \quad (4.40b)$$

$$x_0 = \text{given} \quad (4.40c)$$

$$x^{\text{low}} \leq x_t \leq x^{\text{high}} \quad (4.40d)$$

$$u^{\text{low}} \leq u_t \leq u^{\text{high}} \quad (4.40e)$$

where

$$z^\top = (u_0^\top, \dots, u_{N-1}^\top, x_1^\top, \dots, x_N^\top) \quad (4.40f)$$

Provided the problem is feasible at all times stability is guaranteed, more specifically the origin is asymptotically stable (Rawlings and Muske, 1993). This is proved by showing that the value function for the whole horizon is a *Lyapunov function* and that this function decays towards the origin.

The proof requires a choice for  $N$ , which is difficult, if not impossible, in practice. A proof like this, and similar stability proofs, should therefore be used to provide insight into problems and solutions rather than precisely define an MPC algorithm.

## 4.5 Nonlinear MPC

Similar to the open loop optimization case the extension from linear MPC to nonlinear MPC is in principle straightforward. We rewrite (4.1) similar to (3.51).

$$\min_{z \in \mathbb{R}^n} f(z) = \sum_{t=0}^{N-1} \frac{1}{2} x_{t+1}^\top Q_{t+1} x_{t+1} + d_{x_{t+1}} x_{t+1} + \frac{1}{2} u_t^\top R_t u_t + d_{u_t} u_t + \frac{1}{2} \Delta u_t^\top R_{\Delta t} \Delta u_t \quad (4.41a)$$

subject to

$$x_{t+1} = g(x_t, u_t) \quad (4.41b)$$

$$x_0, u_{-1} = \text{given} \quad (4.41c)$$

$$x^{\text{low}} \leq x_t \leq x^{\text{high}} \quad (4.41d)$$

$$u^{\text{low}} \leq u_t \leq u^{\text{high}} \quad (4.41e)$$

$$-\Delta u^{\text{high}} \leq \Delta u_t \leq \Delta u^{\text{high}} \quad (4.41f)$$

where

$$Q_t \succeq 0 \quad (4.41g)$$

$$R_t \succeq 0 \quad (4.41h)$$

$$R_{\Delta t} \succeq 0 \quad (4.41i)$$

The state feedback linear MPC algorithm is given by Algorithm 7. In the output feedback case an estimate of the state is needed, i.e.,  $\hat{x}_t$ .

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### Algorithm 7 Nonlinear MPC with state feedback

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**for**  $t = 0, 1, 2, \dots$  **do**

    Get the current state  $x_t$ .

    Solve the optimization problem (4.41) on the prediction horizon from  $t$  to  $t + N$  with  $x_t$  as the initial condition.

    Apply the first control move  $u_t$  from the solution above.

**end for**

---

It is beyond the scope of this note to discuss NMPC in any detail. We will however provide a few comments.

The key difference, and in fact the only difference between (4.1) and (4.41), is the nonlinear model (4.41b). This turns the convex QP problem

for linear MPC into a nonlinear and nonconvex problem. This complicates solution procedures significantly since an NLP solver is needed instead of a QP solver. This is exactly the same change as discussed in conjunction with dynamic optimization of nonlinear systems in (3.51).

In the output feedback case state estimation plays a key role. Estimators for nonlinear dynamic models tend to be more complex than for linear models and an exact solution of the nonlinear state estimation problem is in fact intractable. Hence, approximations must be made. The Kalman filter, as discussed in Section 4.2.3, is also used for nonlinear systems. However, alternatives that address nonlinear behavior directly and thereby improve performance have been developed. The *extended Kalman filter (EKF)* was proposed in order to apply the Kalman filter to nonlinear spacecraft navigation problems (Bellantoni and Dodge, 1967) and is probably the most used method in applied nonlinear state estimation. The EKF is based on a linearization of a nonlinear model at each time step. Hence, it uses the time varying Jacobian matrices, cf. (3.6), to compute a new filter matrix at each time step. Another approach, which approximates the nonlinear filter solution more accurately, is the *unscented Kalman filter (UKF)*, see Julier and Uhlmann (2004). The MHE, which was discussed in Section 4.2.3, is also applicable to nonlinear systems.

## 4.6 Comments

There are many aspects of dynamic optimization and MPC, some of which have been covered in the earlier sections. Subsequently we comment on some important topics to provide further insight.

### 4.6.1 The control hierarchy and MPC

A control system is often structured according to layers as shown in Figure 4.8. The controlled system, at the bottom, provides realtime data to the control system through sensors and communication channels to controllers in the next layer, the *regulatory control layer*. The controllers are conventional controllers, often *PID controllers*<sup>28</sup>, and they are used to control properties like pressure, flow rate, temperature, power, voltage, speed and heading depending on the application. These controllers are embedded in a *distributed control system (DCS)* or industrial *programmable logic controllers (PLCs)*. The regulatory control layer needs setpoints, for instance for flow rates, temperatures, power, voltages, position and heading. These setpoints are sup-

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<sup>28</sup>A PID controller will often only activate its proportional and integral action.

plied by the *advanced process control (APC)* layer where the use of MPC is spreading rapidly (Qin and Badgwell, 2003). Hence, MPC controls a process through a regulatory layer and may communicate with the DCS through a network based on for instance the *OPC communication protocol*.

In Figure 4.8 the upper scheduling and optimization layer may include production plans of different products based on some manual analysis technique or as an output from an optimization application. Such applications are usually based on static models and the oil optimization case in Example 2 is an example of this.

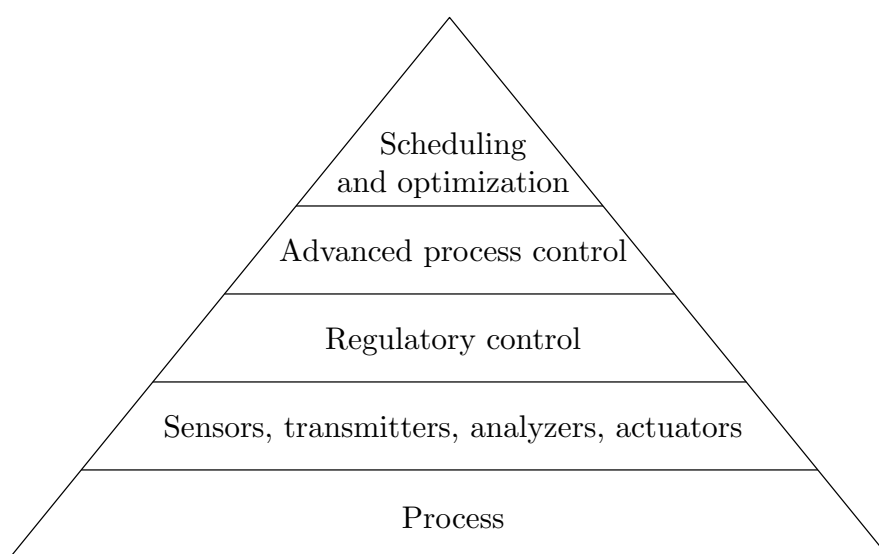


Figure 4.8: Typical control hierarchy.

As mentioned earlier MPC applications are located in the APC layer of Figure 4.8. The information flow is such that measurements  $y_t$  are passed from the lower regulatory control layer while setpoints ( $\gamma_t$ ) and (possibly) varying constraints are transferred from the upper scheduling and optimization layer. The output from the MPC application, i.e., the computed control inputs ( $u_t$ ), are sent to the lower layer as setpoints for low level controls.

To elaborate further, the sampling frequency decreases upwards in the hierarchy. Regulatory control may compute new control inputs every second while the APC sampling time is a minute or more, and rescheduling may be done once a day.

The control hierarchy is valid for many sectors and two examples are given below.

- In refineries an optimization application based on static models may be used to schedule production for a whole refinery. Such an applica-

tion solves a large LP or NLP problem where models of the complete refinery are included. The APC layer will include linear MPC applications for controlling key parts of the refinery like distillation columns. The APC layer also includes simpler control strategies, e.g., heuristic based control logic. The solution from the upper optimization problem provides some of the setpoints and constraints that are used in the APC layer. The regulatory control layer includes a large number of PID controller for controlling basic variables like flow rates, pressures, temperature, levels and concentrations where the setpoints are supplied by the controllers in the APC layer.

- A ship or an airplane may use an optimization application to decide on a route from A to B. This information is transferred to an MPC application. Hence, the MPC controller may be used to keep the ship or plane close to the initial trajectory, or it may even change the trajectory based on recent information. The latter may for instance save time or fuel. The regulatory control layer will include basic controllers, e.g., for heading control and pitch control.

To home in on MPC applications a specific example is presented below.

**Example 14** (MPC applications as part of a large control system)

To elaborate we use Figure 4.9, which shows the Ekofisk complex in the North Sea. Much of this large installation is controlled by ABB DCS systems that communicate with sensors and actuators, performs control operations with PID controllers or other logic, include procedures for start-up and shut-down of systems, to mention some important functions. Thus, the regulatory layer is in its entirety implemented in the DCS system, and safety critical controllers are for instance placed in this layer. Sensor data from more than 10000 tags are sampled every second. Some data is filtered and transferred to an external realtime data base, in this case a PI realtime database<sup>29</sup>. This data is used for different purposes.

If future MPC applications were installed, they would most probably communicate with a realtime database, rather than the a DCS system directly, by reading appropriate tags from the database and checking data quality before solving the appropriate optimization problems. Subsequently the result, i.e., the control input, would be written to the PI database. This data is available to the DCS system, which can read it and adjust the appropriate setpoints. Since the MPC applications are non-critical, communication requirements are limited and the OPC protocol is typically used. The field

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<sup>29</sup>The PI realtime database is a OSIsoft product.



operators and field engineers would observe the MPC applications through their conventional *graphical user interface (GUI)*, i.e., there is no need for additional screen pictures. It should be remembered, however, that a control specialist might need special access to the MPC applications to reconfigure the controllers by for instance changing constraints or models.

It may be added that MPC applications are rare in the upstream oil and gas business, i.e., production systems that include oil and gas wells, manifolds and pipelines, and topside processes<sup>30</sup>. MPC technology has however a significant potential in this area, similar to the process industries. Thus, MPC is also expected to penetrate this sector.  $\triangle$

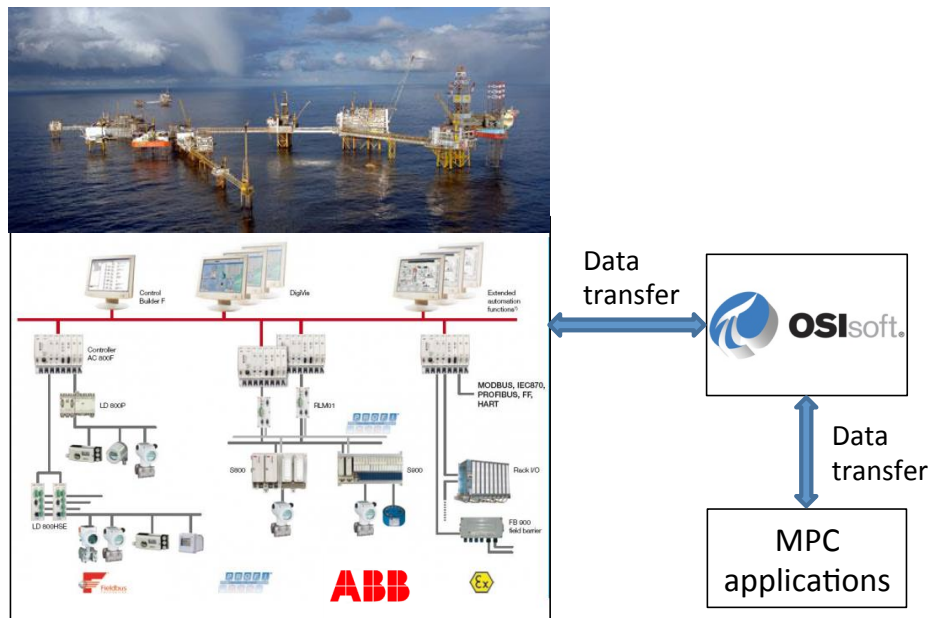


Figure 4.9: This figure shows the Ekofisk offshore complex. ABB DCS systems control part of this large offshore production system where some data is stored in PI realtime databases. An probable architecture for a future MPC application is included.

The APC layer may be missing, meaning that no automatic high-level controllers are in use. In this case low-level setpoints are set manually by operators instead of through APC applications.

The above seems to allude to the fact that MPC is unsuited for safety critical applications and for fast applications where the sampling time is

<sup>30</sup>Topside processes include gas oil water separators, pumps, scrubbers, compressors etc, and the key function is to separate reservoir fluid into gas, oil and water.

in the millisecond region or even faster. This is, however, untrue and there is currently much research on moving MPC into safety critical and/or fast applications. There are alternative solutions. One is obviously to embed MPC applications in the DCS or PLC, which by design use highly reliable software, communication protocols and hardware. Another option is tailored hardware. See Ling et al. (2008) and Jerez et al. (2011) for a couple of examples of how to run MPC algorithms on *field-programmable gate arrays (FPGA)* to gain speed by massive parallelization. The latter paper also addresses the issue of power consumption, which can be critical in certain applications. This line of development opens new application areas for MPC like robotics, power generation and distribution, vehicles, and low-level control such as stabilizing controllers.

### 4.6.2 MPC performance

An important reason for the industrial success of MPC is improved performance through increased disturbance rejection and better tracking performance. Hence, MPC helps systems comply with tighter performance specifications from worldwide competition and increasing constraints from environmental and safety considerations, and thereby improves economy. We will now elaborate further on this.

A well tuned MPC application usually improves control as illustrated in Figure 4.10. In this case, after the MPC controller is switched on, control performance improves since disturbance rejection increases significantly. Now, given an operational limit, which must be satisfied, a constraint supplied by the upper optimization layer may be increased due to improved control as shown towards the end of the time interval. This is often called “squeeze and shift”. The operational limit may for instance be temperature in an exothermic reactor, oil production rate, or the distance between a vessel and an oil platform. In all these cases improved MPC performance may improve the economics of the reactor, the oil production system or vessel operations. In terms of the control hierarchy in Figure 4.8 this discussion is related to the two upper layers where the MPC controller receives some of its inputs, in particular some of its constraints, from the top layer.

Most processes are limited by constraints. A distillation column, for instance, may be constrained by boiler capacity, limits on the pressure differential across the column, or product purity specifications. It is difficult, if not impossible, to dynamically track the constraints that limit production without resorting to mathematical optimization. In this sense MPC provides a tool that automatically adjusts the control strategy to push against, and thereby exploit, the constraints that limit production according to the chosen

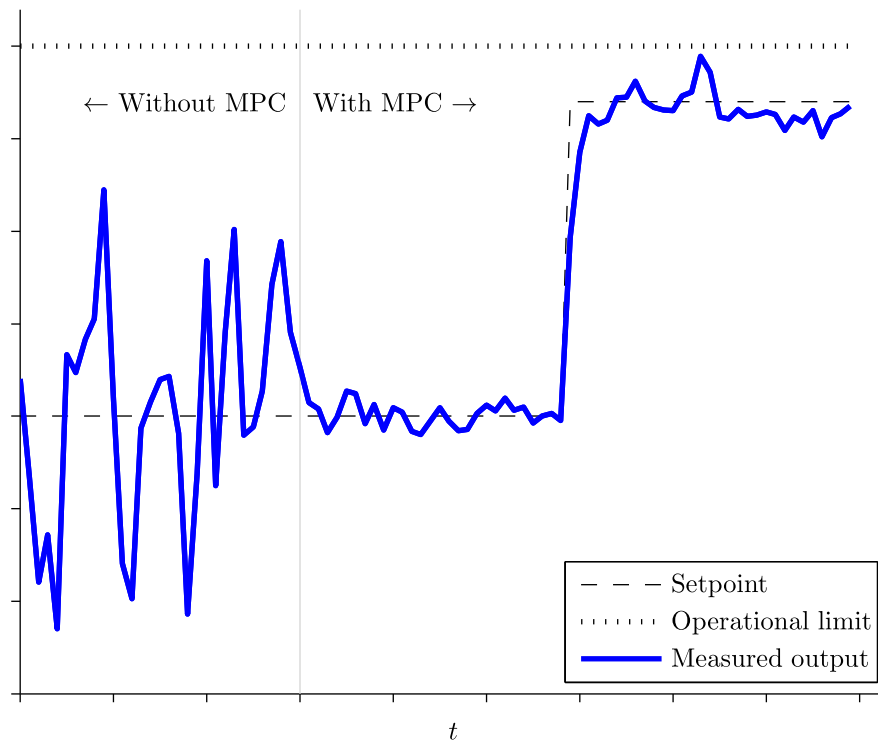


Figure 4.10: An MPC controller improves performance and may therefore operate closer to an operational limit. This is often called “squeeze and shift”. The setpoint is provided by a higher level in the control hierarchy.

objective function.

MPC performance also depends on the performance of the regulatory controllers. It is always important to have well tuned controllers in the regulatory control layer, e.g., well tuned PID controllers. The effect of this is shown in Figure 4.11 and it is similar to the “squeeze and shift” effect discussed above. The key observation is thus that all low level controller must be well tuned to gain the full benefit of MPC.

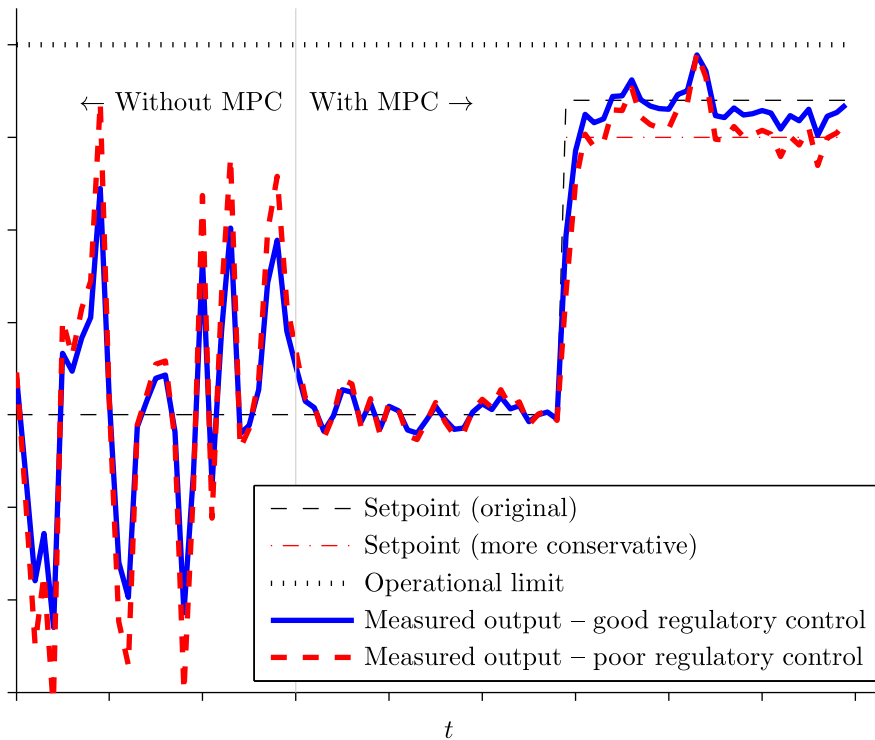


Figure 4.11: The performance of an MPC controller depends on low-level controller tuning. This figure compares the performance of a system with well tuned low-level controllers from Figure 4.10 and with poorly tuned low-level controllers (the red dashed output). Since the poor tuning of the regulatory controllers lead to larger oscillations it is necessary to use a more conservative setpoint to ensure that the operational limit is respected. The setpoints are provided by a higher level in the control hierarchy.

### 4.6.3 Feedforward control

*Feedforward control* is an efficient way to improve performance when disturbance measurements are available. This is commonly used in regulatory

control where for instance a level controller for a tank may include a feedforward term from an upstream measurement. Thereby the level control can react before a disturbance affects the tank level. Feedforward action can easily be embedded into MPC by extending the dynamic model with a disturbance model. Focussing on linear MPC, cf. (4.1), feedforward is included by extending the linear model (4.1b) as shown below

$$x_{t+1} = A_t x_t + B_t u_t + C v_t \quad (4.42)$$

where  $v_t$  are measured disturbances. The downside of this is a more complex model since a disturbance model  $C v_t$  is needed. However, this extension hardly affects computation time.

One example of feedforward MPC is its use in distillation column control where the inflow rate, and possibly composition and temperature, is used as feedforward measurements.

#### 4.6.4 MPC models

An MPC controller needs a dynamic model. In this note we have focussed on state space models. In principle there are two approaches to modeling; *experimental models*<sup>31</sup> and *first principles models*<sup>32</sup>. Experimental models are developed from data and are popular in linear MPC applications, in particular the *step response model* since this is a model that is easy to identify from experimental data. These models are usually formulated in an *input output form* rather than a state space model.

First principles models usually require more development cost than experimental models (Foss et al., 1998). They do, however, have certain distinct advantages. First, since these models are based on physics, e.g., mass and energy conservation laws, they tend to provide better prediction capabilities than experimental models, in particular beyond the operating range covered by experimental data. Second, physics based models need less data for model identification and validation.

#### 4.6.5 Practical MPC formulations

The basic linear MPC problem (4.1) is not used directly in industrial applications. We have already discussed several extensions like ensuring feasibility at all times and feedforward control. There are many other extension, some of which are listed below.

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<sup>31</sup>Experimental models are also called black box models and data driven models.

<sup>32</sup>First principles models are also called physics based models, mechanistic models and white box models.

*Control input blocking* is commonly used and shown in Figure 4.12. It is useful to compare this figure with the upper part of Figure 4.1 where the number of control input decision variables is  $N \cdot n_u$ . Control input blocking reduces this number considerably.  $N$  may typically be 20 while the number of control moves with control input blocking may be 4 or 5. Control input blocking reduces runtime. This reduction may however be marginal for linear MPC since the number of states is much larger than the control input dimension as discussed in Section 3.3. Practice has shown, however, that control input blocking works well. In NMPC applications control input blocking may reduce runtime significantly and may therefore be an important contribution to secure a robust NMPC application.

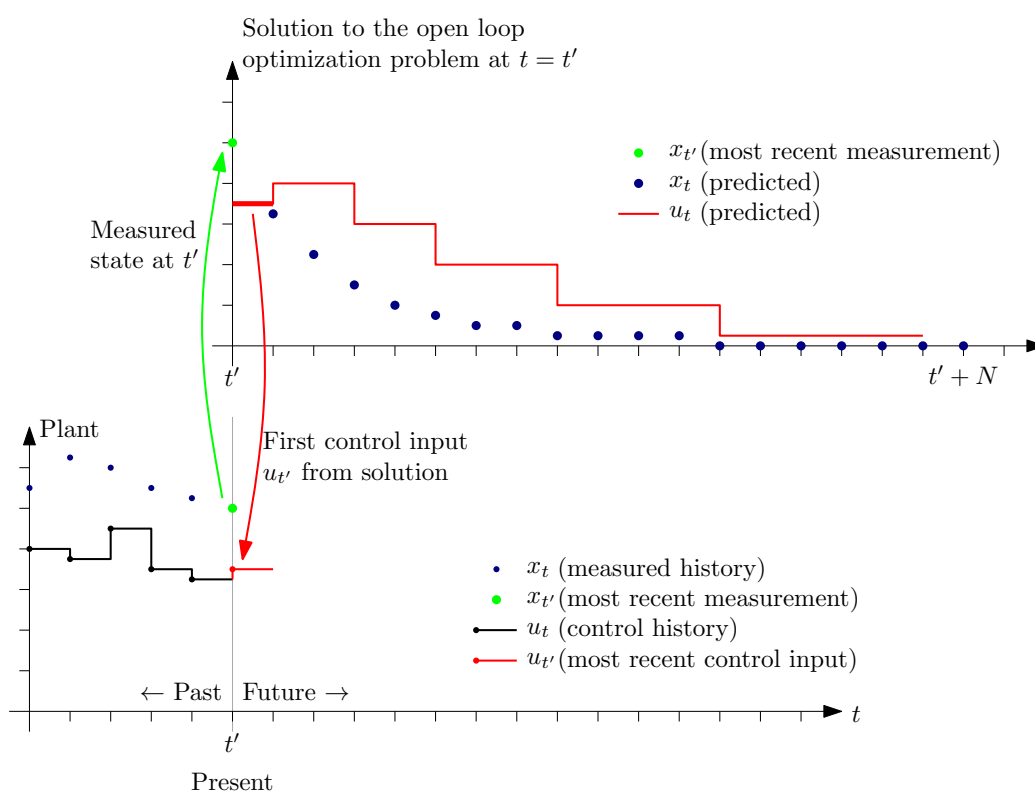


Figure 4.12: Illustration of the MPC with control input blocking.

Some terms that are extensively used in practice are explained below.

- *CV* refers to a controlled variable. This is equal to  $\gamma_t$ , which has been discussed several times in this note. We emphasize again that *CV*, or  $\gamma_t$ , differs from the measured data  $y_t$  as discussed in conjunction with (4.13).

- $MV$  refers to a manipulated variable and is the equivalent of the control input  $u_t$ .
- $DV$  refers to a disturbance variable and equals the measured disturbance  $v_t$  in (4.42).

# Acknowledgments

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